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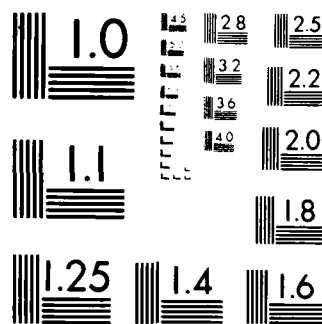
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**TECHNICAL REPORT BRL-TR-2624**

**SIDE MOMENT EXERTED BY A TWO-COMPONENT  
LIQUID PAYLOAD ON A SPINNING PROJECTILE**

**Charles H. Murphy**

**December 1984**

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## I. INTRODUCTION

The prediction of the complete moment exerted by a spinning liquid payload on a spinning and coning projectile has been a problem of considerable interest to the Army for some time. For a fully spinning liquid, the linear side moment was first computed by Stewartson<sup>1</sup> for an inviscid payload by use of eigenfrequencies determined by the fineness ratio of the cylindrical container. Wedemeyer<sup>2</sup> introduced boundary layers on the walls of the container and was able to determine viscous corrections for Stewartson's eigenfrequencies, which could then be used in Stewartson's side moment calculation. Murphy<sup>3</sup> then completed the linear boundary layer theory by including all pressure and wall shear contributions to the liquid-induced side moment. The Stewartson-Wedemeyer eigenvalue calculations have been improved for low Reynolds numbers by Kitchens *et al.*<sup>4</sup> through the replacement of the cylindrical wall boundary approximation by a linearized Navier-Stokes approach. Next, Gerber *et al.*<sup>5-6</sup> extended this linearized NS technique to compute better side moment coefficients for Reynolds numbers less than 10,000. Finally, the roll moment for a fully spun-up liquid was computed by Murphy.<sup>7-8</sup>

1. K. Stewartson, "On the Stability of a Spinning Top Containing Liquid," *Journal of Fluid Mechanics*, Vol. 5, Part 4, September 1959, pp. 577-592.
2. E. H. Wedemeyer, "Viscous Correction to Stewartson's Stability Criterion," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Report No. 1325, June 1966. (AD 489687)
3. C. H. Murphy, "Angular Motion of a Spinning Projectile With a Viscous Liquid Payload," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Memorandum Report ARBRL-MR-03194, August 1982. (AD A118676). (See also *Journal of Guidance, Control, and Dynamics*, Vol. 6, July-August 1983, pp. 280-286.)
4. C. W. Kitchens, Jr., N. Gerber, and R. Sedney, "Oscillations of a Liquid in a Rotating Cylinder: Solid Body Rotation," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Technical Report BRL-TR-02081, June 1978. (AD A057759)
5. N. Gerber, R. Sedney, and J. M. Bartos, "Pressure Moment on a Liquid-Filled Projectile: Solid Body Rotation," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Technical Report ARBRL-TR-02422, October 1982. (AD A120567)
6. N. Gerber and R. Sedney, "Moment on a Liquid-Filled Spinning and Nutating Projectile: Solid Body Rotation," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Technical Report ARBRL-TR-02470, February 1983. (AD A125332)
7. C. H. Murphy, "Liquid Payload Roll Moment Induced by a Spinning and Coning Projectile," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Technical Report ARBRL-TR-02521, September 1983. (AD A133681) (See also AIAA Paper 83-2142, August 1983.)
8. C. H. Murphy, "A Relationship Between Liquid Roll Moment and Liquid Side Moment," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Memorandum Report ARBRL-MR-03347, April 1984. (AD A140658)

An important limitation of this work has been the restriction to a single liquid in the payload. Scott<sup>9</sup> has derived relations for eigenfrequencies for two inviscid liquids and obtained fair experimental agreement. For Scott's inviscid liquids the tangential perturbation velocities have discontinuous jumps at the two-liquid interface.

In this report we will consider two viscous liquids, although we will restrict our consideration of viscosity to boundary layers near the cylindrical walls and near the two-liquid interface. The remainder of the liquid will be considered to be inviscid. Under these assumptions, side moment coefficients, as well as eigenfrequencies, will be computed.

## II. LIQUID BOUNDARY CONDITIONS

Two coordinate systems will be used in this report: the nonrolling aeroballistic  $\tilde{X}\tilde{Y}\tilde{Z}$  system whose  $\tilde{X}$ -axis is fixed along the missile's axis of symmetry and the inertial  $XYZ$  system whose  $X$ -axis is tangent to the trajectory at time zero. Both coordinate systems have origins at the center of the cylindrical payload cavity, which is assumed to be at the center of mass of the projectile. Location in the cavity can be specified in the aeroballistic system by the cylindrical coordinates  $\tilde{x}, \tilde{r}, \tilde{\theta}$  and in the inertial system by  $x, r, \theta$ . The boundary of the cavity is given by  $\tilde{x} = \pm c$  and  $\tilde{r} = a$  where  $2c$  is the height of the cavity and  $2a$  is its diameter. The projectile is assumed to be performing a coning motion of amplitude  $K_1(t)$  and phase angle  $\phi_1(t)$ . If  $\tilde{\alpha}$  and  $\tilde{\beta}$  are the angles of attack and side-slip of the missile's axis with respect to the trajectory (the  $X$ -axis),

$$\begin{aligned}\tilde{\beta} + i \tilde{\alpha} &= K_1 e^{i\phi_1} \\ &= \hat{K} e^{s\phi}\end{aligned}\tag{2.1}$$

where

$$\phi = \dot{\phi} t$$

$$s = (\varepsilon + i) \tau$$

$$\hat{K} = K_1(0) e^{i\phi_1(0)}$$

---

9. W. E. Scott, "The Inertial Wave Frequency Spectrum in a Cylindrically Confined, Inviscid, Incompressible Two Component Liquid," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Report No. 1609, September 1972. (AD 752439). (See also Physics of Fluids, Vol. 16, No. 1, pp. 9-12, January 1973.)

$$\tau = \dot{\phi}_1 / \dot{\phi}$$

$$\tau \dot{\phi} = \dot{K}_1 / K_1,$$

and  $\dot{\phi}$  is the axial component of the angular velocity relative to inertia axes and is assumed to be positive and constant. Linear relations between cylindrical coordinates in the two coordinate systems were derived in Reference 3:

$$\tilde{x} = x - r K_1 \cos(\phi_1 - \theta) = x - r R \{ \hat{K} e^{S\hat{\phi}} \} \quad (2.2)$$

$$\tilde{r} = r + x K_1 \cos(\phi_1 - \theta) = r + x R \{ \hat{K} e^{S\hat{\phi}} \} \quad (2.3)$$

$$\tilde{\theta} = \theta + (x/r) K_1 \sin(\phi_1 - \theta) = \theta - (x/r) R \{ i \hat{K} e^{S\hat{\phi}} \}, \quad (2.4)$$

where  $R\{ \} = [\{ \} + \{ \bar{\} \}]/2$  is the real part of a complex quantity.

The two liquids have densities  $\rho_1$  and  $\rho_2$  ( $\rho_1 \geq \rho_2$ ) and kinematic viscosities  $\nu_1$  and  $\nu_2$ . When the liquids are fully spun up and  $K_1 = 0$ , liquid 1 occupies the cylindrical annular region  $b_1 \leq r \leq a$  and liquid 2 occupies a cylindrical annular region  $b_2 \leq r \leq b_1$ . The fill ratio,  $f$ , is the ratio of the volume of the annular region containing both liquids to that of the complete cylinder, i.e.,  $1 - (b_2/a)^2$ . The surface  $r = b_2$  is either a free surface or the surface of a rigid central rod. The free surface boundary will be considered in this report while the central rod will be discussed in Appendix A. For a fully filled cylinder,  $b_2 = 0$  and  $f = 1$ .

When the cylinder is forced to perform a coning motion, the interface between the liquids is located at

$$r_1 = b_1 (1 + \eta_1) \quad (2.5)$$

where

$$|\eta_1(x, \theta, t)| \ll 1,$$

and the free inner surface is located at

$$r_2 = b_2 (1 + \eta_2) \quad (2.6)$$

where

$$|\eta_2(x, \theta, t)| \ll 1.$$

The velocity components in the two liquids have a very simple form.

$$v_{xj} = R \{u_{js} e^{s\phi - i\theta}\} a; \quad (2.7)$$

$$v_{rj} = R \{v_{js} e^{s\phi - i\theta}\} a; \quad (2.8)$$

$$v_{\phi j} = \frac{1}{r} + R \{w_{js} e^{s\phi - i\theta}\} a; \quad (2.9)$$

where  $j = 1, 2$ .

The fluid pressure, however, has a more complicated form:

$$\begin{aligned} p &= p_0 & 0 \leq r \leq r_2 \\ &= p_0 + \rho_2 \frac{1}{2} \left[ \frac{r^2 - b_2^2}{2} \right] + R \{p_{2s} e^{s\phi - i\theta}\} \rho_2 a^2 & r_2 \leq r \leq r_1 \\ &= p_0 + \rho_2 \frac{1}{2} \left[ \frac{b_1^2 - b_2^2}{2} \right] + \rho_2 \frac{1}{2} \left[ \frac{r^2 - b_1^2}{2} \right] & (2.10) \\ &\quad + R \{p_{1s} e^{s\phi - i\theta}\} \rho_1 a^2 & r_1 \leq r \leq a \end{aligned}$$

If we assume the small perturbation of the interface surface has the same form as the perturbation velocities,

$$\eta_1 = R \{\eta_{1s}(x) e^{s\phi - i\theta}\}. \quad (2.11)$$

By use of Eqs. (2.3, 2.11), the equation of the interface surface is

$$\begin{aligned} F(x, r, \phi, t) &= r - b_1 - R \{b_1 \eta_{1s} e^{s\phi - i\theta}\} \\ &= 0. \end{aligned} \quad (2.12)$$

At the interface, the two liquids have the same velocity, i.e., the velocity of the interface itself.

$$\therefore \frac{dF}{dt} = V_{xj} \frac{\partial F}{\partial x} + V_{rj} \frac{\partial F}{\partial r} + \frac{V_{\theta j}}{r} \frac{\partial F}{\partial \theta} + \frac{\partial F}{\partial t} = 0 \quad (2.13)$$

When only linear terms are retained, this reduces to

$$b_1 \eta_{1s}(x) = \frac{a v_{1s}(b_1, x)}{s - i} = \frac{a v_{2s}(b_1, x)}{s - i} \quad (2.14)$$

Similarly, the perturbation of the inner surface has the form

$$b_2 \eta_{2s}(x) = \frac{a v_{2s}(b_2, x)}{s - i} \quad (2.15)$$

where

$$\eta_2 = R \{ \eta_{2s} e^{s\phi - i\theta} \}$$

In addition to three continuous velocity components at the interface, we will require the pressure and the two viscous shears to be continuous at the interface. Equations (2.10, 2.14) yield a simple pressure relation at the interface:

$$p_{1s}(b_1, x) + \frac{b_1 v_{1s}(b_1, x)}{a(s - i)} = \rho_{21} \left[ p_{2s}(b_1, x) + \frac{b_1 v_{2s}(b_1, x)}{a(s - i)} \right] \quad (2.16)$$

where  $\rho_{21} = \rho_2 / \rho_1$ .

If only velocity gradients normal to the interface are considered, the continuous viscous shear assumptions imply that

$$\mu_1 \frac{\partial u_{1s}(b_1, x)}{\partial r} = \mu_2 \frac{\partial u_{2s}(b_1, x)}{\partial r} \quad (2.17)$$

$$\mu_1 \frac{\partial w_{1s}(b_1, x)}{\partial r} = \mu_2 \frac{\partial w_{2s}(b_1, x)}{\partial r} \quad (2.18)$$

At the free surface, the pressure is constant and the viscous shears are zero.

$$p_{2s}(b_2, x) + \frac{b_2 v_{2s}(b_2, x)}{a(s-i)} = 0 \quad (2.19)$$

$$\mu_2 \frac{\partial u_{2s}(b_2, x)}{\partial r} = 0 \quad (2.20)$$

$$\mu_2 \frac{\partial w_{2s}(b_2, x)}{\partial r} = 0. \quad (2.21)$$

Finally, at the cylinder surface the liquid must have the rigid body motion of the cylinder.

$$u_{1s} = (s-i) \hat{K} \quad (2.22)$$

$$v_{1s} = -(s-i) (x/a) \hat{K} \quad (2.23)$$

$$w_{1s} = i(s-i) (x/a) \hat{K}. \quad (2.24)$$

### III. THE INVISCID SOLUTION

The perturbation functions are written as sums of viscous and inviscid parts.

$$u_{js} = u_{jsi} + u_{jss} \quad w_{js} = w_{jsi} + w_{jss} \quad (3.1)$$

$$v_{js} = v_{jsi} + v_{jss} \quad p_{js} = p_{jsi} + p_{jss}.$$

The differential equations for the inviscid functions of each liquid are the same as those for a single liquid and the solutions have the same form.<sup>3</sup>

More specifically, the pressure and velocity perturbations are expressed as the sum of products of functions of  $x$  and functions of  $r$ . The functions of  $x$  are  $1$ ,  $x/a$ ,  $\sin(\lambda_{jk} x/a)$ , and  $\cos(\lambda_{jk} x/a)$  where

$$\lambda_{jk} = (\pi k/2) [1 + \delta_{cj}] ; \quad k = 1, 3, 5 \dots (2N_k - 1) \quad (3.2)$$

$$\delta_{cj} = \frac{-(a/c)(1+i)}{2\sqrt{2}(1+is)} \left\{ \frac{1-is}{\sqrt{3+is}} + \frac{i(3+is)}{\sqrt{1-is}} \right\} \text{Re}_j^{-1/2} \quad (3.3)$$

$$\text{Re}_j = \frac{a^2 \phi}{v_j}. \quad (3.4)$$

The specific expressions for pressure and velocity functions are given in Table 1.

TABLE 1. INVISCID PERTURBATION FUNCTIONS\*

$$p_{jsi} = - [(i-s)^2 (x/c)(r/a) + \sum R_{jk}(r) \sin(\lambda_{jk} x/c)] (c/a) \hat{K}$$

$$u_{jsi} = -[(i-s)(r/a) + (i-s)^{-1} \sum R_{jk} \lambda_k \cos(\lambda_{jk} x/c)] \hat{K}$$

$$v_{jsi} = [(i-s)^2 (i+s)^{-1} (x/c) + \sum R_{vjk} \sin(\lambda_{jk} x/c)] (c/a) \hat{K}$$

$$w_{jsi} = [-i (i-s)^2 (i+s)^{-1} (x/c) + \sum R_{wjk} \sin(\lambda_{jk} x/c)] (c/a) \hat{K}$$

$$R_{jk} = E_{jk} J_1(\hat{r}) + F_{jk} Y_1(\hat{r})$$

$$R_{vjk} = [(s-i) a R'_{jk} - 2i(a/r) R_{jk}] S^{-1}$$

$$R_{wjk} = - [2a R'_{jk} + i(s-i) (a/r) R_{jk}] S^{-1}$$

$$\hat{r} = \hat{\lambda}_{jk} r/c$$

$$\hat{\lambda}_{jk}^2 = - \left[ \frac{S}{(s-i)^2} \right] \lambda_{jk}^2$$

$$S = s^2 - 2s + 3.$$

If  $v_1 \neq v_2$ , the  $\lambda_{jk}$ 's for the same  $k$  are not the same, the trigonometric functions on opposite sides of the liquid interface are slightly different, and the interface boundary conditions require a special least squares process. In the body of this report, we will use a single  $\lambda_k$  determined by an average kinematic viscosity,  $v_a$ .

$$\lambda_k = (\pi k/2) [1 + \delta_{c1} (v_a/v_1)^{1/2}] \quad (3.5)$$

\*The conditions for the  $E_{jk}$ 's and  $F_{jk}$ 's are given in Section 7. Note that the definitions of  $E_{jk}$  and  $F_{jk}$  in Table 1 differ from the  $E_k$  and  $F_k$  of Reference 1.



where

$$v_a = \frac{v_1 (a^2 - b_1^2) + v_2 (b_1^2 - b_2^2)}{a^2 - b_2^2}.$$

In Appendix B, a much more accurate treatment of unequal viscosities will be described.

#### IV. THE VISCOUS SOLUTION

In Reference 3 the viscous parts of the perturbation variables were important only in a small region near the cylinder wall and the endwalls, and these functions were computed by the use of unsteady boundary layer equations in these regions. It is reasonable to expect that the viscous parts can also have contributions near the liquid interface and that derivatives in the radial direction are much larger than those in the circumferential or axial directions. Thus, we will assume that the viscous functions away from the endwalls satisfy the same equations as those for the cylindrical wall boundary layers.<sup>3</sup>

$$(s - i) w_{jsv} = a^2 \text{Re}_j^{-1} \frac{\partial^2 w_{jsv}}{\partial r^2} \quad (4.1)$$

$$(s - i) u_{jsv} = a^2 \text{Re}_j^{-1} \frac{\partial^2 u_{jsv}}{\partial r^2} \quad (4.2)$$

$$a \frac{\partial p_{jsv}}{\partial r} = 2 w_{jsv}. \quad (4.3)$$

The solutions to Eqs. (4.1 - 4.3) are

$$w_{1sv} = w_{10} e^{\frac{r-a}{a \delta_{a1}}} + w_{11} e^{\frac{-(r-b_1)}{a \delta_{a1}}} \quad (4.4)$$

$$w_{2sv} = w_{21} e^{\frac{r-b_1}{a \delta_{a2}}} + w_{22} e^{\frac{-(r-b_2)}{a \delta_{a2}}} \quad (4.5)$$

$$u_{1sv} = u_{10} e^{\frac{r-a}{a \delta_{a1}}} + u_{11} e^{\frac{-(r-b_1)}{a \delta_{a1}}} \quad (4.6)$$

$$u_{2sv} = u_{21} e^{\frac{r - b_1}{a \delta_{a2}}} + u_{22} e^{\frac{-(r - b_2)}{a \delta_{a2}}} \quad (4.7)$$

$$p_{1sv} = 2 \delta_{a1} \left[ w_{10} e^{\frac{r - a}{a \delta_{a1}}} - w_{11} e^{\frac{-(r - b_1)}{a \delta_{a1}}} \right] \quad (4.8)$$

$$p_{2sv} = 2 \delta_{a2} \left[ w_{21} e^{\frac{r - b_1}{a \delta_{a2}}} - w_{22} e^{\frac{-(r - b_2)}{a \delta_{a2}}} \right], \quad (4.9)$$

where  $\delta_{aj} = \left[ \frac{1 + i}{\sqrt{2} (1 + is)} \right] \text{Re}_j^{-1/2},$

and the eight coefficients  $u_{jk}, w_{jk}$  are functions of  $x$ . Four conditions on the coefficients come from the continuity of tangential velocities and shears [Eqs. (2.17 - 2.18)] at the interface.

$$\Delta w_{si} + w_{10} \epsilon_1 + w_{11} - w_{21} - w_{22} \epsilon_2 = 0 \quad (4.10)$$

$$\Delta u_{si} + u_{10} \epsilon_1 + u_{11} - u_{21} - u_{22} \epsilon_2 = 0 \quad (4.11)$$

$$w_{10} \epsilon_1 - w_{11} = N (w_{21} - w_{22} \epsilon_2) \quad (4.12)$$

$$u_{10} \epsilon_1 - u_{11} = N (u_{21} - u_{22} \epsilon_2) \quad (4.13)$$

where

$$\Delta w_{si} = [w_{1si} - w_{2si}]_{r = b_1}$$

$$\Delta u_{si} = [u_{1si} - u_{2si}]_{r = b_1}$$

$$\epsilon_1 = e^{\frac{b_1 - a}{a \delta_{a1}}}$$

$$\epsilon_2 = e^{\frac{b_2 - b_1}{a \delta_{a2}}}$$

$$N = \rho_{21} \sqrt{v_2/v_1}.$$

Four more conditions come from the no-slip condition at the cylindrical wall [Eqs. (2.22, 2.24)] and the no-shear condition of the free surface [Eqs. (2.20 - 2.21)] .

$$w_{1si}(a, x) + w_{10} + w_{11} \epsilon_1 = i(s - i)\hat{K}(x/a) . \quad (4.14)$$

$$u_{1si}(a, x) + u_{10} + u_{11} \epsilon_1 = (s - i) \hat{K} . \quad (4.15)$$

$$w_{21} \epsilon_2 - w_{22} = 0 . \quad (4.16)$$

$$u_{21} \epsilon_2 - u_{22} = 0 . \quad (4.17)$$

Eqs. (4.10 - 4.17) can now be used to determine the eight coefficient functions. If the total liquid occupies an annular region that is thicker than ten boundary layer thicknesses, the product  $\epsilon_1 \epsilon_2$  is quite small and can be neglected. The resulting expressions for the coefficient functions are given in Table 2. If the liquid interface is more than ten boundary layer thicknesses from both the cylindrical surface and the free surface, both  $\epsilon_1$  and  $\epsilon_2$  are very small and can be neglected in Table 2.

Eqs. (4.8 - 4.9) can be used in conjunction with Eqs. (4.12, 4.16) to yield general relations for the viscous perturbation pressures at the three boundaries.

$$p_{2sv}(b_2, x) = 0 . \quad (4.18)$$

$$p_{1sv}(b_1, x) = \rho_{21} p_{2sv}(b_1, x) . \quad (4.19)$$

$$p_{1sv}(a, x) = 2 \delta_{a1} (w_{10} - w_{11} \epsilon_1) . \quad (4.20)$$

TABLE 2. VISCOUS COEFFICIENT FUNCTIONS FOR INTERNAL FREE SURFACE.

$$w_{10} = \{[1 + N + (1 - N) \epsilon_2^2] w_a + N \epsilon_1 \Delta w_{si}\} D^{-1}$$

$$w_{11} = \{(1 - N) \epsilon_1 w_a - N (1 - \epsilon_2^2) \Delta w_{si}\} D^{-1}$$

$$w_{21} = \{2 \epsilon_1 w_a + (1 + \epsilon_1^2) \Delta w_{si}\} D^{-1}$$

$$w_{22} = \epsilon_2 \Delta w_{si} D^{-1}$$

$$u_{10} = \{[1 + N + (1 - N) \epsilon_2^2] u_a + N \epsilon_1 \Delta u_{si}\} D^{-1}$$

$$u_{11} = \{(1 - N) \epsilon_1 u_a - N (1 - \epsilon_2^2) \Delta u_{si}\} D^{-1}$$

$$u_{21} = \{2 \epsilon_1 u_a + (1 + \epsilon_1^2) \Delta u_{si}\} D^{-1}$$

$$u_{22} = \epsilon_2 \Delta u_{si} D^{-1}$$

$$v_{10} = \{[1 + N + (1 - N) \epsilon_2^2] v_a + N \epsilon_1 \Delta^* \} D^{-1}$$

$$v_{11} = \{-(1 - N) \epsilon_1 v_a + N (1 - \epsilon_2^2) \Delta^* \} D^{-1}$$

$$v_{21} = \{2 \epsilon_1 v_a + (1 + \epsilon_1^2) \Delta^* \} D^{-1}$$

$$v_{22} = -\epsilon_2 \Delta^* D^{-1}$$

where

$$w_a = i (s - i) (x/a) \hat{K} - w_{1si} (a, x)$$

$$u_a = (s - i) \hat{K} - u_{1si} (a, x)$$

$$v_a = -(s - i) (x/a) \hat{K} - \left[ \frac{\partial (r v_{1si})}{\partial r} \right]_{r=a}$$

$$D = 1 + N + (1 - N) (\epsilon_1^2 + \epsilon_2^2)$$

$$\Delta^* = \left[ \frac{\partial (r v_{1si})}{\partial r} - \frac{\partial (r v_{2si})}{\partial r} \right]_{r=b_1}$$

In order to compute the viscous radial velocity, we must use an inequality involving the magnitude of a complex exponential. From the definition of  $\delta_{aj}$

$$\left| \exp \left\{ -\frac{\Delta r}{a \delta_{aj}} \right\} \right| = \exp \left\{ \frac{-2^{-1/2} \Delta r}{a |\delta_{aj}|} \right\} \quad (4.21)$$

$$\therefore \left| \frac{\Delta r}{a} \exp \left\{ -\frac{\Delta r}{a \delta_{aj}} \right\} \right| = 2^{1/2} |\delta_{aj}| z e^{-z} < |\delta_{aj}| \quad (4.22)$$

where  $z = 2^{-1/2} \frac{\Delta r}{a} |\delta_{aj}|^{-1} > 0$ .

Equations (4.4 - 4.7) can now be substituted in the continuity equation. The results can then be integrated and simplified by use of Inequality (4.22) and neglecting  $|\delta_{aj}|^2$  terms.

$$r v_{1sv} = a \delta_{a1} \left[ v_{10} e^{\frac{r-a}{a \delta_{a1}}} + v_{11} e^{\frac{-(r-b_1)}{a \delta_{a1}}} \right] \quad (4.23)$$

$$r v_{2sv} = a \delta_{a2} \left[ v_{21} e^{\frac{r-b_1}{a \delta_{a2}}} + v_{22} e^{\frac{-(r-b_2)}{a \delta_{a2}}} \right] \quad (4.24)$$

where  $v_{10} = i w_{10} - a u'_{10}$

$$v_{11} = -[i w_{11} - b_1 u'_{11}]$$

$$v_{21} = i w_{21} - b_1 u'_{21}$$

$$v_{22} = -[i w_{22} - b_2 u'_{22}]$$

Eqs. (4.23 - 4.24) can now be used in conjunction with Eqs. (4.11, 4.13 - 4.17) to give relations for the radial viscous velocity at the three boundaries.

$$v_{2sv}(b_2, x) = 0 \quad (4.25)$$

$$\begin{aligned} v_{1sv}(b_1, x) &= \rho_{21} v_{2sv}(b_1, x) \\ &= \rho_{21} [v_{21} + \epsilon_2 v_{22}] (a/b_1) \delta_{a2} \end{aligned} \quad (4.26)$$

$$v_{1sv}(a, x) = [v_{10} + v_{11} \epsilon_1] \delta_{a1} \quad (4.27)$$

where  $v_{jk}$  are given in Table 2 (relation (4.22) was used to simplify entries in this table).

#### V. INVISCID BOUNDARY CONDITIONS

In the previous section, we used eight of the twelve liquid boundary conditions to determine the viscous perturbations in terms of the inviscid perturbations. We will now completely determine the inviscid perturbation by use of the remaining four conditions--Eqs. (2.16, 2.19, 2.23) and  $v_{1s} = v_{2s}$  at the interface. These conditions can be simply stated by use of Eqs. (4.18, 4.19, 4.25, 4.26):

at  $r = b_1$

$$p_{1si} + \frac{b_1 v_{1si}}{a(s-i)} = \rho_{21} \left[ p_{2si} + \frac{b_1 v_{2si}}{a(s-i)} \right] \quad (5.1)$$

$$v_{1si} = v_{2si} + (1 - \rho_{21}) v_{2sv} \quad (5.2)$$

at  $r = b_2$

$$p_{2si} + \frac{b_2 v_{2si}}{a(s-i)} = 0 \quad (5.3)$$

at  $r = a$

$$v_{1si} + v_{1sv} = (i - s) (x/a) \hat{K} \quad (5.4)$$

Eqs. (5.1 - 5.4) with  $v_{1sv}$  and  $v_{2sv}$  set equal to zero were used by Scott<sup>9</sup> to obtain eigenfrequencies for a completely inviscid liquid payload. As can be seen from Table 1, for each  $k$  four constants must be determined to completely determine the inviscid perturbation functions, i.e.,  $E_{1k}$ ,  $E_{2k}$ ,  $F_{1k}$ ,  $F_{2k}$ . (For the special case of 100% filled cylinder ( $b_2 = 0$ ),  $F_{2k}$  is zero and

instead of  $4N_k$  constants only  $3N_k$  constants remain to be determined.) To obtain these conditions, we fit  $(x/c)$  to a series in  $\sin(\lambda_k x/c)$  by least squares

$$x/c = \sum a_k \sin(\lambda_k x/c). \quad (5.5)$$

Next, Eq. (5.5) and the corresponding expansions for the pressure and velocity functions from Table 1 are substituted in Eqs. (5.1-5.4) and coefficients are equated.

$$\begin{aligned} R_{1k}(b_1) - \rho_{21} R_{2k}(b_1) - (b_1/a)[R_{v1k}(b_1) - \rho_{21} R_{v2k}(b_1)](s-i)^{-1} \\ = \frac{(1 - \rho_{21}) s^2 (i - s)}{i + s} (b_1/a) a_k \end{aligned} \quad (5.6)$$

$$R_{v1k}(b_1) - R_{v2k}(b_1) - (1 - \rho_{21}) \delta_{a2} R_k^* = (1 - \rho_{21}) \epsilon_1 \delta_{a2} A_1 a_k \quad (5.7)$$

$$R_{2k}(b_2) - (b_2/a)(s-i)^{-1} R_{v2k}(b_2) = \frac{s^2 (i - s)}{i + s} (b_2/a) a_k \quad (5.8)$$

$$R_{v1k}(a) - A_2 \delta_{a1} a R'_{v1k}(a) + \epsilon_1 N \delta_{a1} R_k^{**} D_0^{-1} = \frac{2s(i-s)}{i+s} a_k, \quad (5.9)$$

where

$$R_k^* = \{(1 + \epsilon_1^2 - \epsilon_2^2) a [R'_{v1k}(b_1) - R'_{v2k}(b_1)]$$

$$- 2 \epsilon_1 (a/b_1) [R_{v1k}(a) + a R'_{v1k}(a)]\} D_1^{-1}$$

$$R_k^{**} = 2 [R_{v1k}(b_1) + b_1 R'_{v1k}(b_1) - R_{v2k}(b_1) - b_1 R'_{v2k}(b_1)]$$

$$A_1 = 4 (a/b_1) \left[ \frac{s(i-s)}{i+s} \right] D_1^{-1}$$

$$A_2 = [1 + N + (1 - N)(\epsilon_2^2 - \epsilon_1^2)] D_0^{-1}$$

$$D_0 = D - \epsilon_{a1} [1 + N - (1 - N)(\epsilon_1^2 - \epsilon_2^2)]$$

$$D_1 = D - (1 - \epsilon_{21})(1 + \epsilon_1^2 - \epsilon_2^2).$$

## VI. LIQUID MOMENT

For coning motion described by Eq. (2.1), the linear liquid pitch and yaw moment is defined to be:<sup>3</sup>

$$M_{LY} + i M_{LZ} = m_L a^{2\frac{1}{2}} \tau (C_{LSM} + i C_{LIM}) \hat{K} e^{is\phi} \quad (6.1)$$

where  $m_L = 2\pi \rho_1 a^2 c$ .

The major components of this liquid moment are due to the pressure on the lateral wall and the endwalls of the container. Lesser components are due to the viscous wall shear on the lateral and endwalls. Thus, the liquid moment coefficient can be given as a sum of four terms. (For simplicity these terms will be computed for the center of the cylinder at the center of mass of the projectile. More complete expressions are given in Reference 3.)

$$\tau (C_{LSM} + i C_{LIM}) = m_{\rho l} + m_{pe} + m_{vl} + m_{ve}. \quad (6.2)$$

By use of Eqs. (2.2 - 2.4) and Eq. (2.10), the linear periodic part of the pressure can be computed in cylinder-fixed coordinates

$$\begin{aligned} \frac{\Delta p_i}{\rho_1 a^{2\frac{1}{2}}} &= R \{ [\tilde{p}_{1si}(\tilde{r}, \tilde{x})] e^{s\phi - i\tilde{\theta}} \} && \text{for } b_1 < \tilde{r} < a \\ &= \epsilon_{21} R \{ [\tilde{p}_{2si}(\tilde{r}, \tilde{x})] e^{s\phi - i\tilde{\theta}} \} && \text{for } b_2 < \tilde{r} < b_1 \end{aligned} \quad (6.3)$$

where  $\tilde{p}_{jsi}(\tilde{r}, \tilde{x}) = p_{jsi}(\tilde{r}, \tilde{x}) - (\tilde{r}\tilde{x}/a^2) \hat{K}$ .

Eq. (6.3) for the inviscid pressure and Eq. (4.8) for the viscous lateral wall pressure can be integrated to yield the pressure moment coefficient on the lateral wall.



$$m_{p\ell} = i (2 a c \hat{K})^{-1} \int_{-c}^c \tilde{x} [\tilde{p}_{1si}(a, \tilde{x}) + p_{1sv}(a, \tilde{x})] d\tilde{x} \quad (6.4)$$

where  $p_{1sv}(a, \tilde{x}) = 2 \delta_{a1} (w_{10} - w_{11} \epsilon_1)$ .

Since the viscous pressure on the endwalls is zero, the expression for the pressure moment coefficient on the endwalls is slightly simpler.

$$m_{pe} = -i (a^2 c \hat{K})^{-1} \left\{ \int_{b_1}^a \tilde{p}_{1si}(\tilde{r}, c) \tilde{r}^2 d\tilde{r} + p_{21} \int_{b_2}^{b_1} \tilde{p}_{2si}(\tilde{r}, c) \tilde{r}^2 d\tilde{r} \right\}. \quad (6.5)$$

The viscous moment coefficient on the lateral wall can be computed by use of Eqs. (4.4) and (4.6).

$$m_{v\ell} = (2ac \hat{K} \text{Re}_1 \delta_{a1})^{-1} \int_{-c}^c [ia(u_{10} - \epsilon_1 u_{11}) + \tilde{x}(w_{10} - \epsilon_1 w_{11})] d\tilde{x}. \quad (6.6)$$

The viscous moment coefficient on the endwalls is a little more difficult to compute since a change in kinematic viscosity can occur across the interface as well as a change in density. The relations of Reference 3 can, however, be used to obtain the following result.

$$m_{ve} = \left( \frac{\sqrt{i+s}}{a^2 \hat{K}} \right) \text{Re}_1^{-1/2} \left[ \int_{b_1}^a w_1(\tilde{r}) \tilde{r} d\tilde{r} + N \int_{b_2}^{b_1} w_2(\tilde{r}) \tilde{r} d\tilde{r} \right] \quad (6.7)$$

where

$$w_j(\tilde{r}) = 2(1+is)(c/a) \hat{K} - w_{jsi}(\tilde{r}, c) + i v_{jsi}(\tilde{r}, c).$$

# III. DISCUSSION

Equations (5.6) and (5.9) yield values of  $E_{1k}$ ,  $E_{2k}$ ,  $\tau_{kn}$ ,  $\sigma_{kn}$  which determine the  $k$  component of the liquid moment. Values of  $s$  that make the four by four determinant of the system zero are called eigenvalues,  $s_{kn}$ , where  $k$  is the axial mode number and  $n$  is the radial mode number. The imaginary parts of the  $s_{kn}$ 's are frequencies,  $\tau_{kn}$ , of the transient motion in the liquid and the real parts are the damping rates of that motion. (For a single liquid,  $\tau_{k1}$  is the smallest  $\tau_{kn}$  and  $\tau_{kn}$  increases monotonically with increasing  $n$ .) When the forced coning motion of the projectile has a frequency near an eigenfrequency, the liquid side moment has a local maximum. For this reason, the eigenfrequencies are of considerable interest to a projectile designer.\*

The equations of this paper have been coded for the VAX 11/780 computer and eigenfrequencies can be computed for specified values of  $c/a$ ,  $Re$ ,  $k$ ,  $\rho_{21}$ ,  $N$ ,  $b_1/a$ , and  $b_2/a$ . Codes for both an interior free surface and rigid rod are available. In Figs. 1 - 3, sample plots of  $\tau_{31}$  are given for a fineness ratio of 3.1 and Reynolds number of 40,000. Each figure plots  $\tau_{31}$  versus the location of the liquid interface for three values of  $\rho_{21}$ .

In Figure 1, we see that for a fully-filled container,  $\tau_{31}$  has the single-liquid value of .035 at  $b_1/a = 0.1$  and reaches a maximum value for  $b_1/a = .75$ . Thus, the maximum change in eigenfrequency occurs when there are approximately equal volumes of the two liquids.

A fill ratio of 98% ( $b_2/a = .141$ ) is considered for a free surface (Fig. 2) and a central rod (Fig. 3). Although there is very little change from the fully-filled case for the free surface, the central rod has a strong effect. For all density ratios, the single-liquid eigenfrequency of .113 occurs for three values of  $b_1/a$  (0, .53, 1) and the maximum effect is at .8.

\*The eigenvalues of the liquid motion for the transient frequencies have the azimuthal dependence  $e^{ik\theta}$  and the radial dependence  $J_n(r)$ , i.e., proportional to  $e^{im\theta}$  ( $m = 1$ ). Eigenvalues with  $m = 0$  are of theoretical interest. The  $m = 0$  eigenvalues for the transient frequencies are given in Appendix D and have been calculated for  $Re = 1000$ .

Scott's experimental data were for  $c/a = 3.127$ ,  $Re_1 = 2 \times 10^4$ ,  $\rho_{21} = .82$ , and  $f = 0.9, 1$ . (The second, third, and fourth columns of Scott's Table I are mis-labeled in Reference 9. In his notation, they should be identified as  $d/c$ ,  $bdc^{-2}$ , and  $adc^{-2}$ .) His data are compared with the theory of this paper in Figure 4, and we see that the maximum error is 14%. In Reference 3 it was found that much better fits could be obtained by using a slightly different value of the fineness ratio. Indeed, effective values of fineness ratio which were 0.5% greater than the measured value would give excellent agreement. In Figure 4 it is shown that a 0.7% greater fineness ratio ( $c/a = 3.150$ ) gives excellent agreement for six different experiments.

An important characteristic of an eigenfrequency is the occurrence of a maximum side moment coefficient for a coning motion with constant damping and a frequency near the eigenfrequency. The theory of this report was used to compute the maximum side moment coefficients for the conditions of Figure 1 and constant amplitude coning motion with frequency near  $\tau_{31}$ . The resulting curves are given in Figure 5 and have a number of interesting properties.

As  $b_1/a$  varies from 0 to 1, the heavier liquid is replaced by the lighter liquid. Since the side moment is defined in terms of the density  $\rho_1$  of the heavier liquid, a requirement for our  $C_{LSM}(b_1/a)$  is that

$$C_{LSM}(1) = \rho_{21} C_{LSM}(0). \quad (7.1)$$

This requirement was satisfied by our calculations. It is important to note that a large change in side moment occurs when the liquid interface is near the cylindrical wall and the interface boundary layer overlaps the wall boundary layer. Therefore, small amounts of heavier liquid can have a large effect on the side moment exerted by a spinning liquid payload.

An interesting feature of the  $\rho_{21} = .4$  side moment coefficient curve is the presence of two small peaks. These are caused by the equality of  $\tau_{31}$  and  $\tau_{52}$  for these locations of the interface. Figure 6 compares the complete dependence of  $\tau_{52}$  on interface location with that of  $\tau_{31}$  for  $\rho_{21} = .4$ . For  $n = 1$  the eigenfrequency has one maximum, while for  $n = 2$  the corresponding eigenfrequency has two maxima, and for small enough density ratio those eigenfrequency curves can intersect.

The coalescence of eigenfrequencies for special interface locations also occurs for the fineness ratio of 4.29, which has been extensively studied by

Figure 7 shows the primary eigenfrequency of interaction  $\omega_{11,3}$  versus  $b_1/a$  for three density ratios. This curve is compared with the single-liquid eigenfrequency  $\omega_{11,3}$  for  $\rho_2/\rho_1 = 21$ , and it has the single-liquid eigenfrequency  $\omega_{11,3}$  for  $\rho_2/\rho_1 = 1$  as a density ratio. Eigenfrequency  $\omega_{12}$  is compared with the single-liquid  $\omega_{12}$  for  $\rho_2/\rho_1 = 1$  in Figure 8. This  $n = 3$  eigenfrequency  $\omega_{12}$  has several intersections with  $\omega_{12}$ . On Figure 9, the eigenfrequency  $\omega_{12}$  is plotted versus  $b_1/a$  for three density ratios and it shows the presence of an eigenfrequency  $\omega_{12}$ .

Measurements of gyroscope damping rate produced by a mixture of oil and water have recently been made by Kyser et al.<sup>11</sup> For a mixture of 15% silicon oil and 85% water, the damping rate is plotted versus  $\omega$  in Figure 10. This mixture is contained in a cylindrical container mounted in the gyroscope. The theoretical side moment can be used to predict the damping rate, and this prediction is shown as the dashed curve. The shape of the curve is good but there is a frequency bias of .0025. This bias corresponds to changing the fineness ratio 0.3% from the actual value of 3.126 to an effective value of 3.135.

#### VIII. SUMMARY

1. A linear boundary layer theory has been developed for a two-liquid payload that is rolling and spinning.
2. The predicted eigenfrequencies and side moments agree well with available experiments except for an unexplained frequency bias.
3. Large changes in side moments can be caused by the presence of a small amount of heavier liquid.
4. For various locations of the liquid interface, pairs of eigenfrequencies can be obtained.

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$Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 1$   
Fully Filled

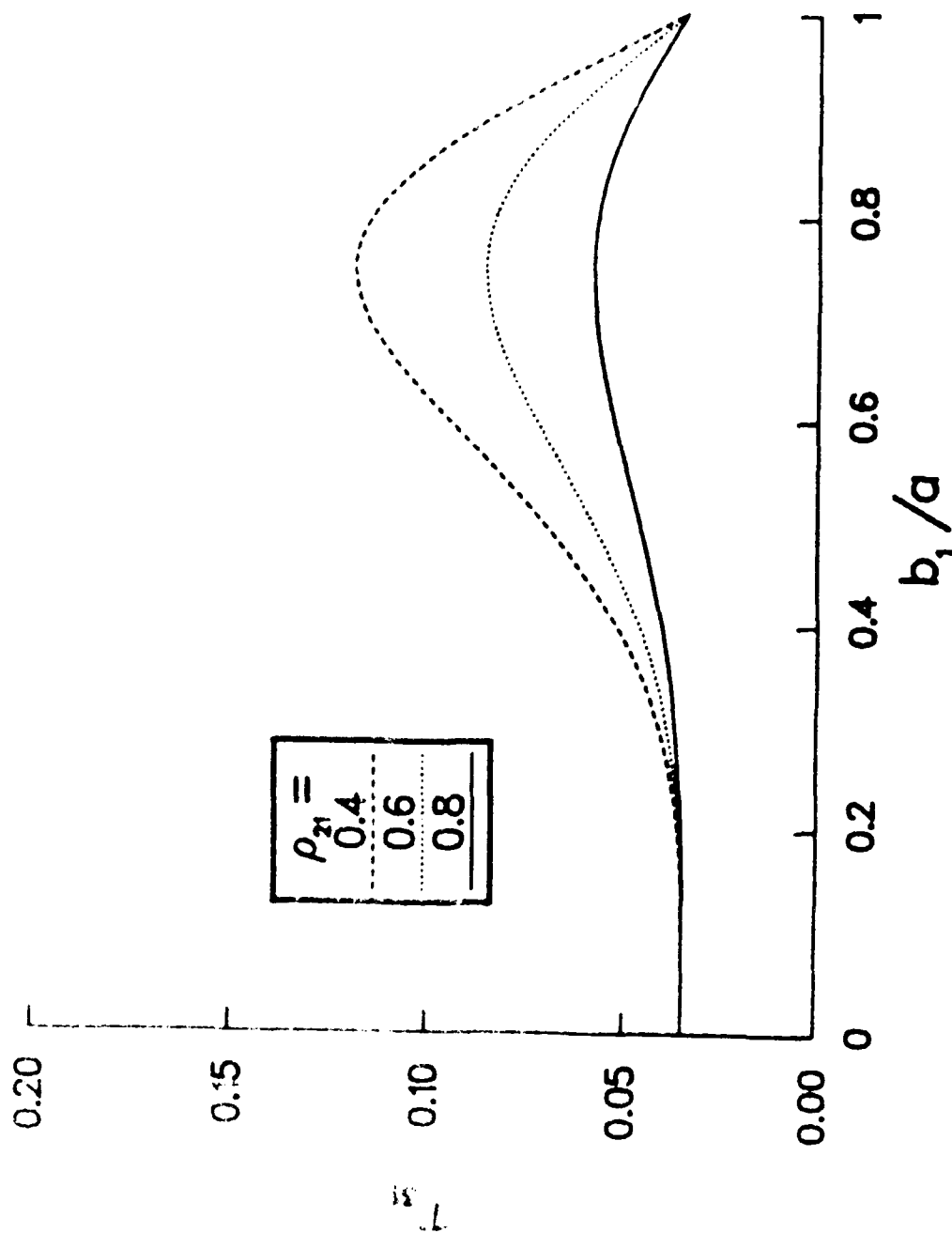


Figure 1.  $r_{31}$  versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 1$  and Various Density Ratios.

$Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 0.98$   
Air Core

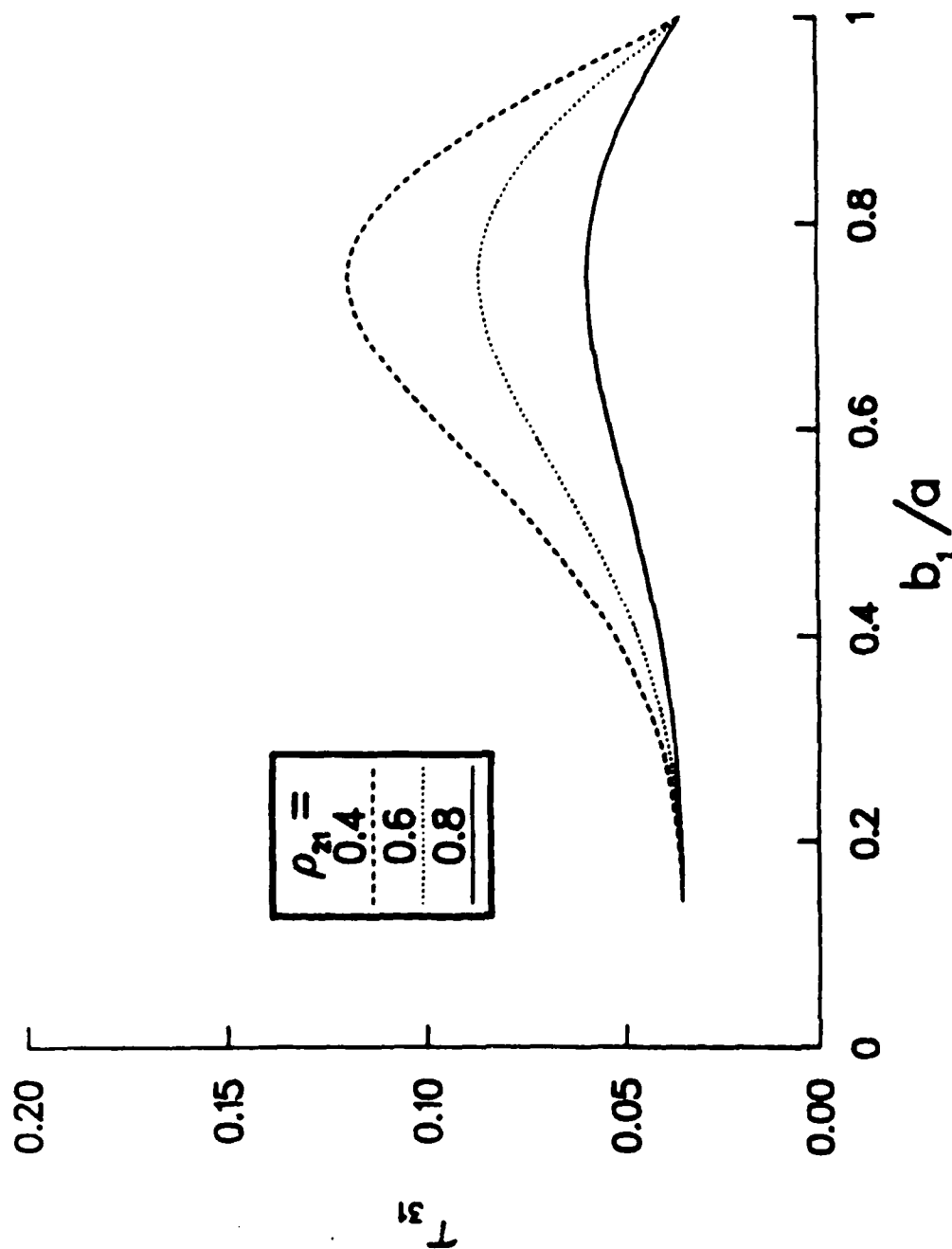


Figure 2.  $r_{31}$  versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = .98$  with a Free Surface and Various Density Ratios.

$Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 0.98$

Central Rod

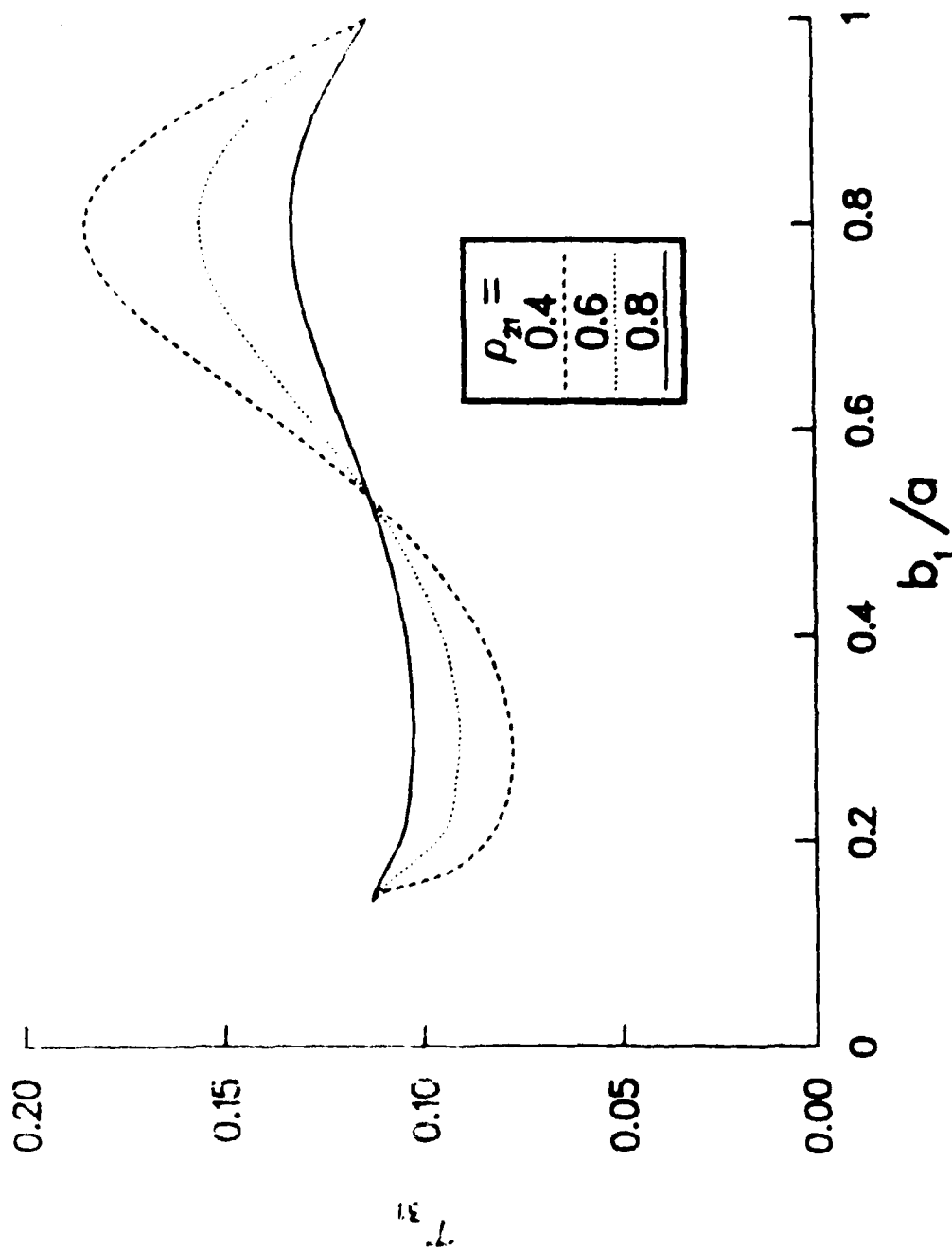


Figure 3.  $f_{31}$  versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = .98$  with a Central Rod and Various Density Ratios.



$$Re_1 = 2 \times 10^6, \rho_{21} = .82$$

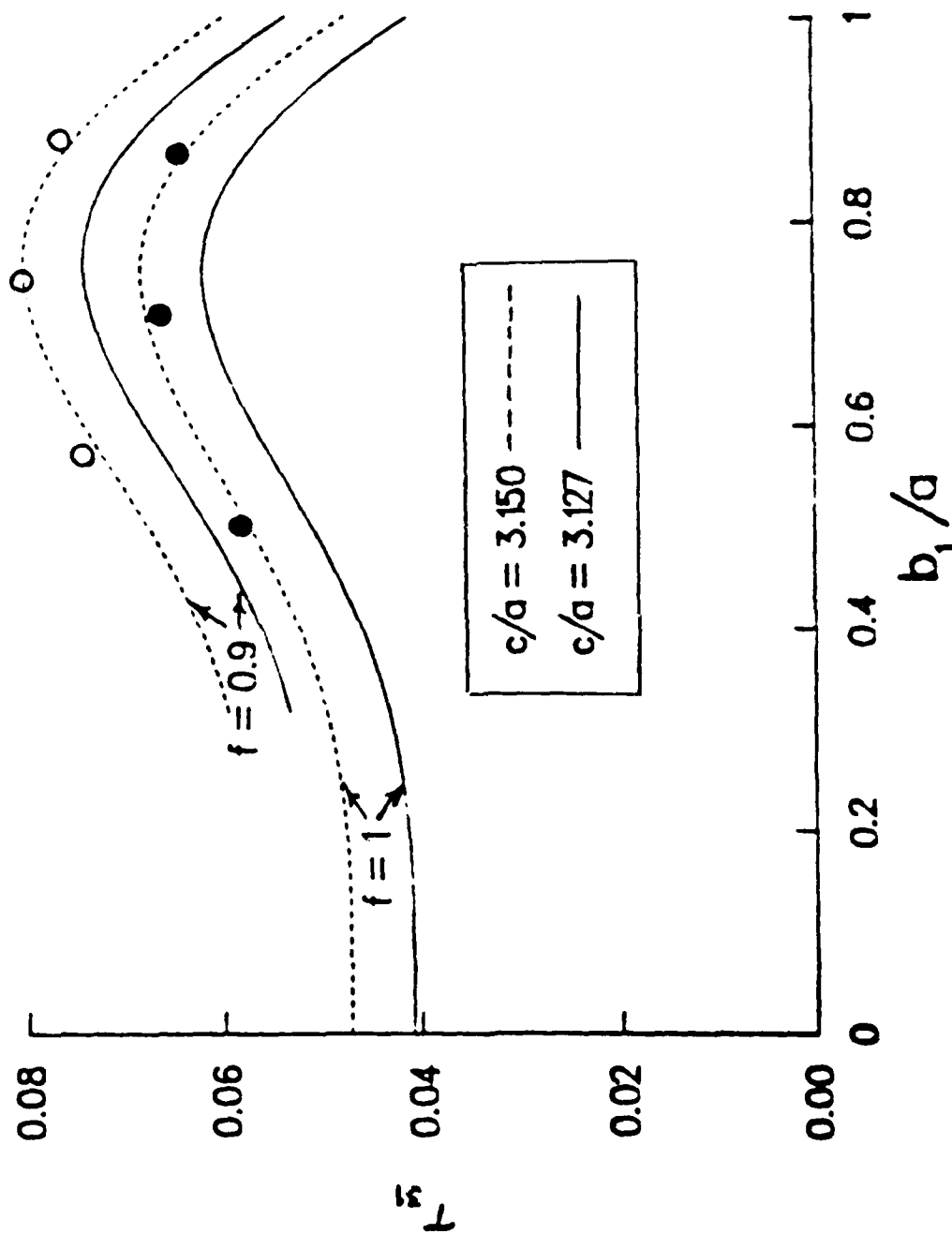


Figure 4.  $\tau_{31}$  versus  $b_1/a$  for  $Re_1 = 2 \times 10^6$ ,  $c/a = 3.127$ ,  $\rho_{21} = .82$  and Various Free Surface Fill Ratios. Experimental Data are from Reference 9.

$$Re_1 = 4 \times 10^4, c/a = 3.1, f = 1$$

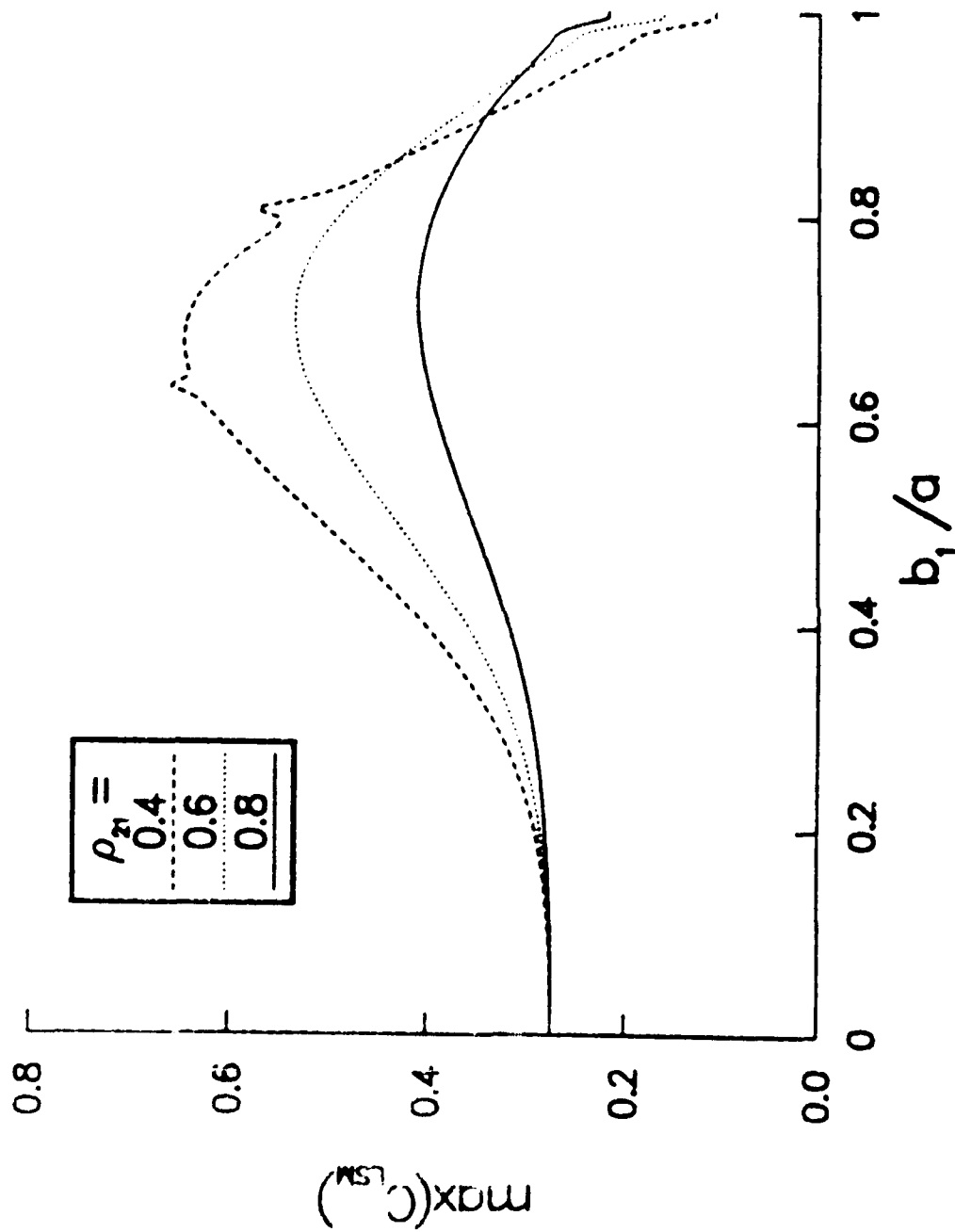


Figure 5.  $\tau_{31}$  Maximum Side Moment Coefficient versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 1$  and Various Density Ratios.

$$Re_1 = 4 \times 10^4, c/a = 3.1, f = 1$$

$$\rho_{21} = 0.4$$

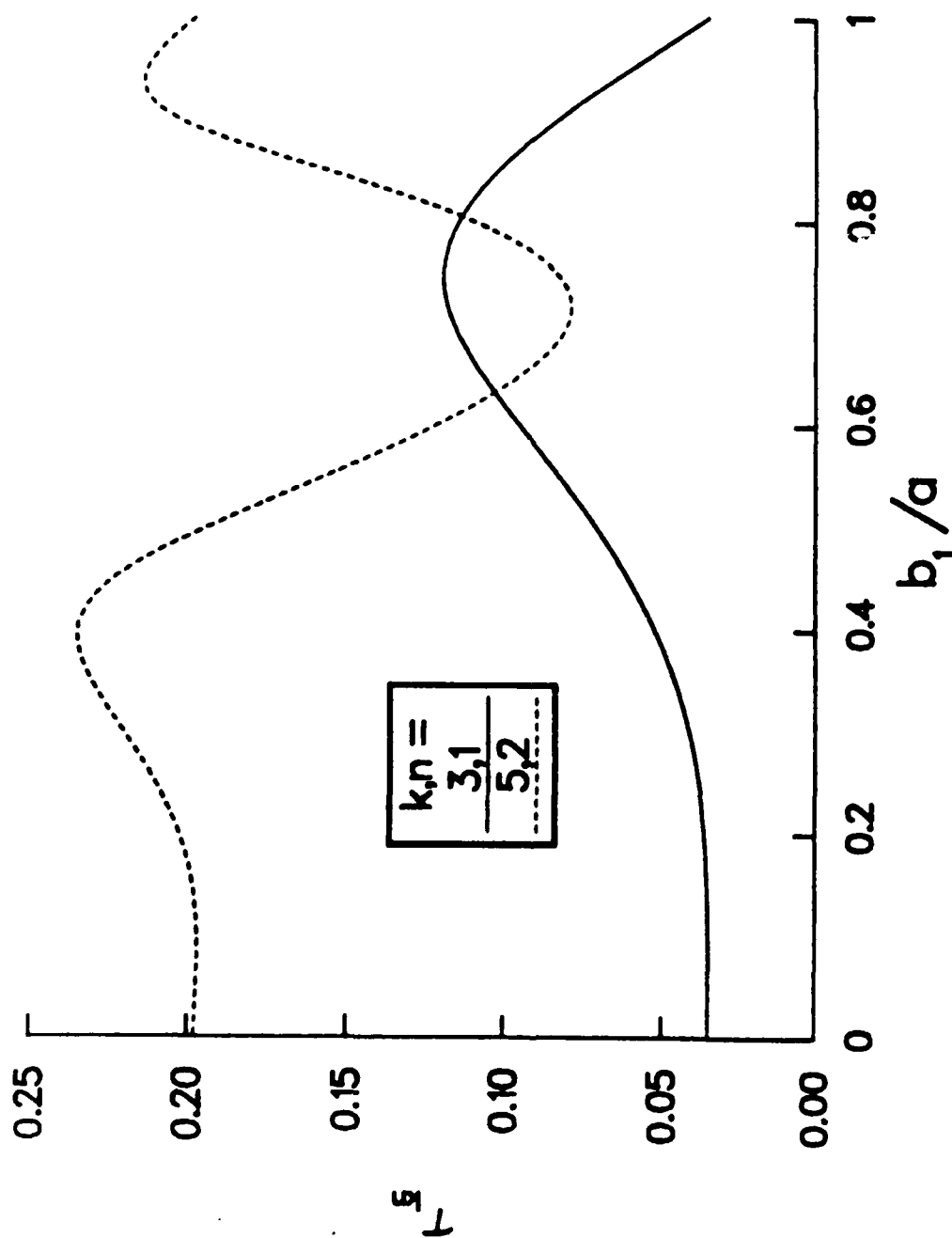


Figure 6.  $\tau_{31}$  and  $\tau_{52}$  versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 1$ ,  $\rho_{21} = .4$ .

$$\text{Re}_1 = 10^\circ, c/a = 4.29, f = 1$$

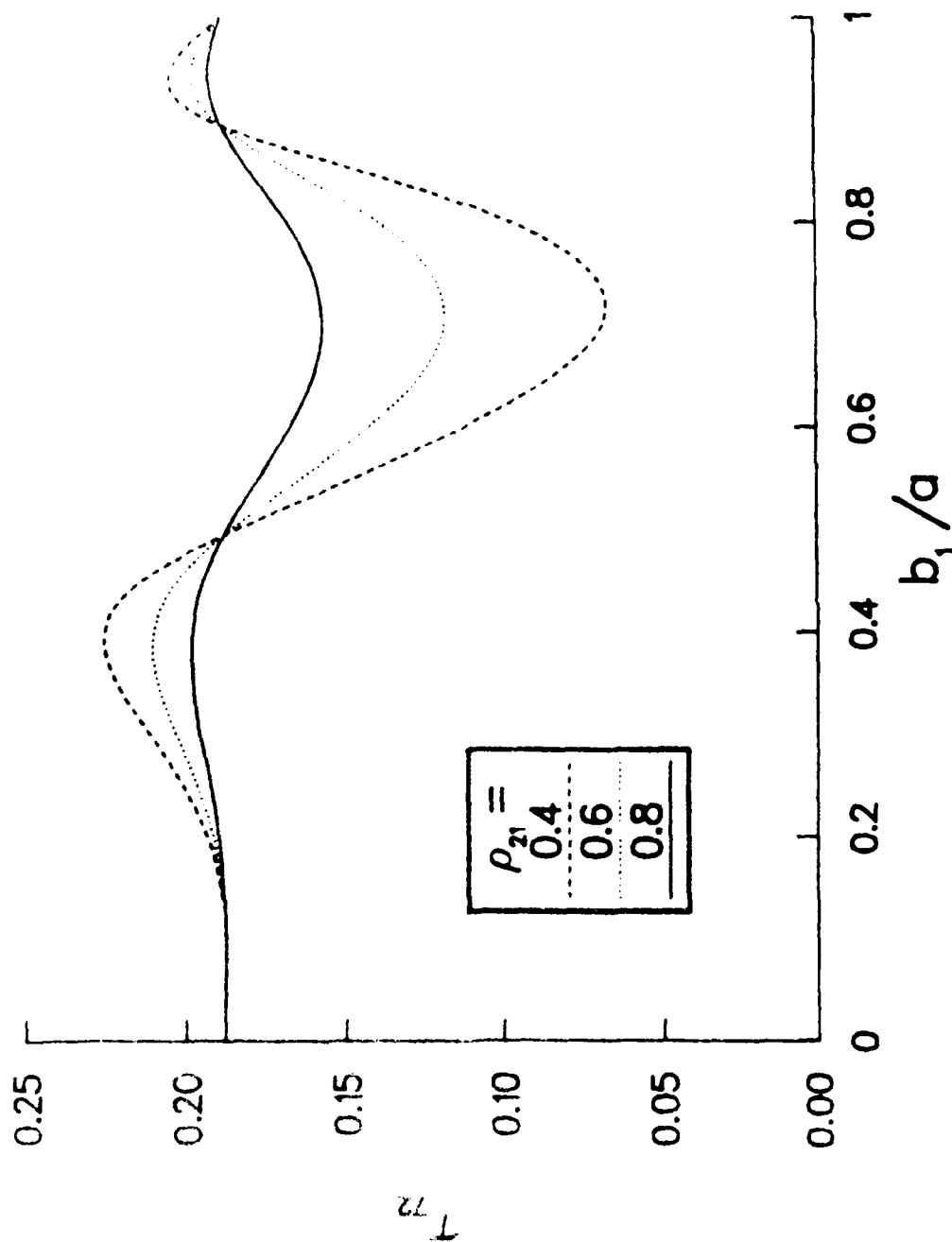


Figure 7.  $\tau_{72}$  versus  $b_1/a$  for  $\text{Re}_1 = 10^\circ$ ,  $c/a = 4.29$ ,  $f = 1$  and Various Density Ratios.

$$\text{Re}_1 = 10^6, c/a = 4.29, f = 1$$

$$\rho_{21} = 0.8$$

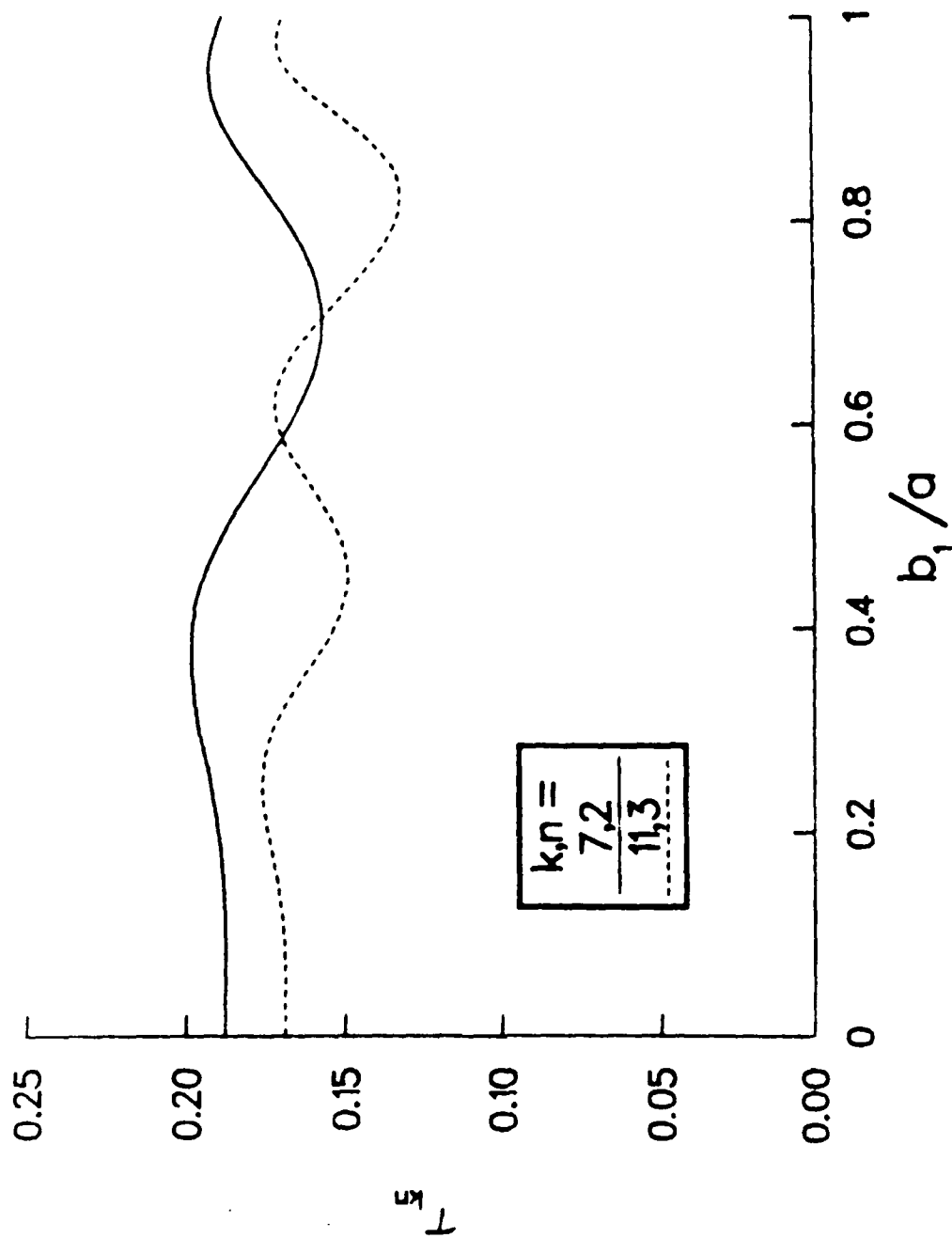


Figure 8.  $\tau_{72}$  and  $\tau_{11,3}$  versus  $b_1/a$  for  $\text{Re}_1 = 10^6$ ,  $c/a = 4.29$ ,  $f = 1$  and  $\rho_{21} = 0.8$ .

$$Re_1 = 10^6, c/a = 4.29, f = 1$$

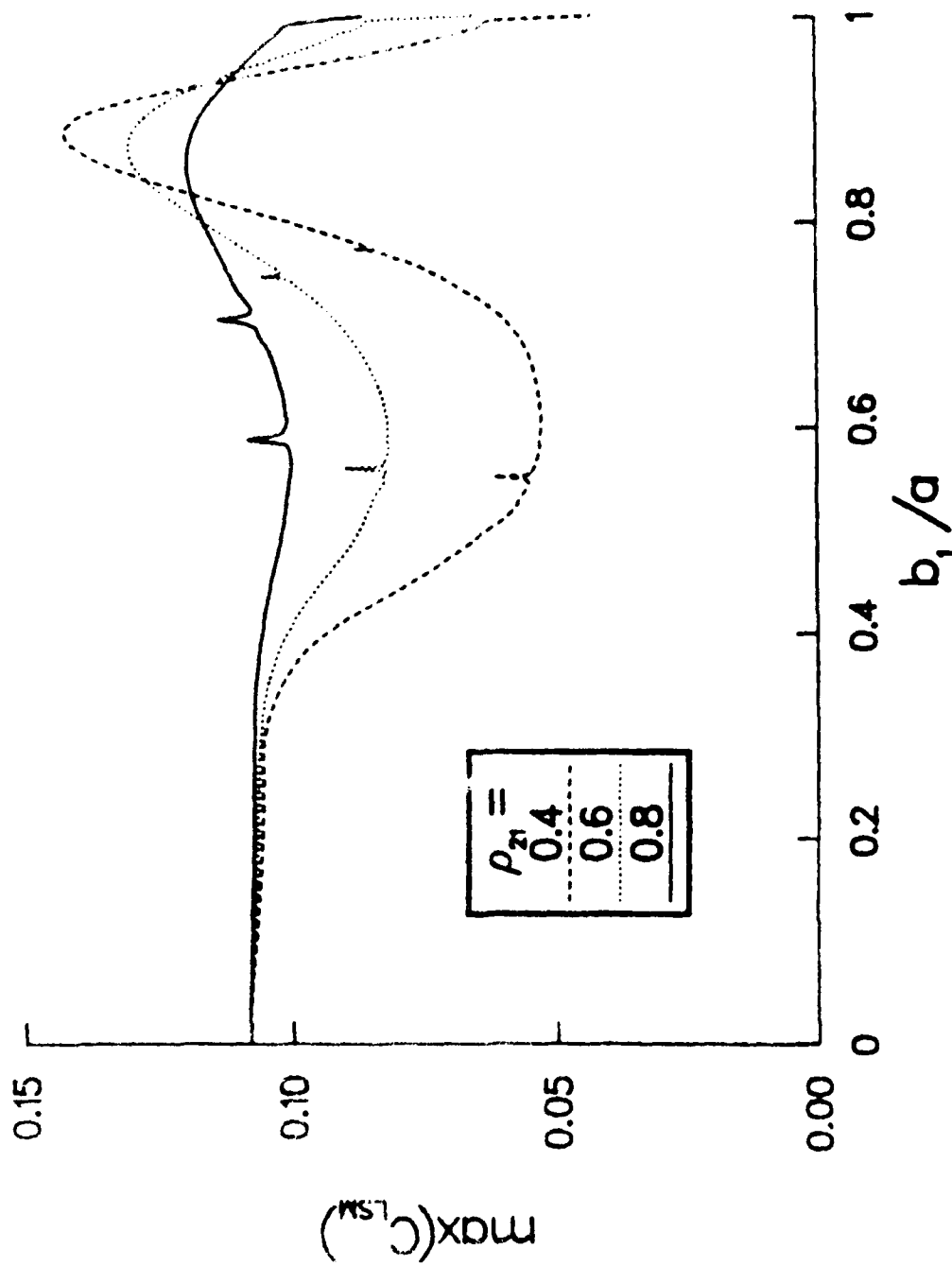


Figure 9.  $\tau_{72}$  Maximum Side Moment Coefficient versus  $b_1/a$  for  $Re_1 = 10^6$ ,  $c/a = 4.29$ ,  $f = 1$  and Various Density Ratios.

# BINARY

RE=534000 OIL/H<sub>2</sub>O=15/85

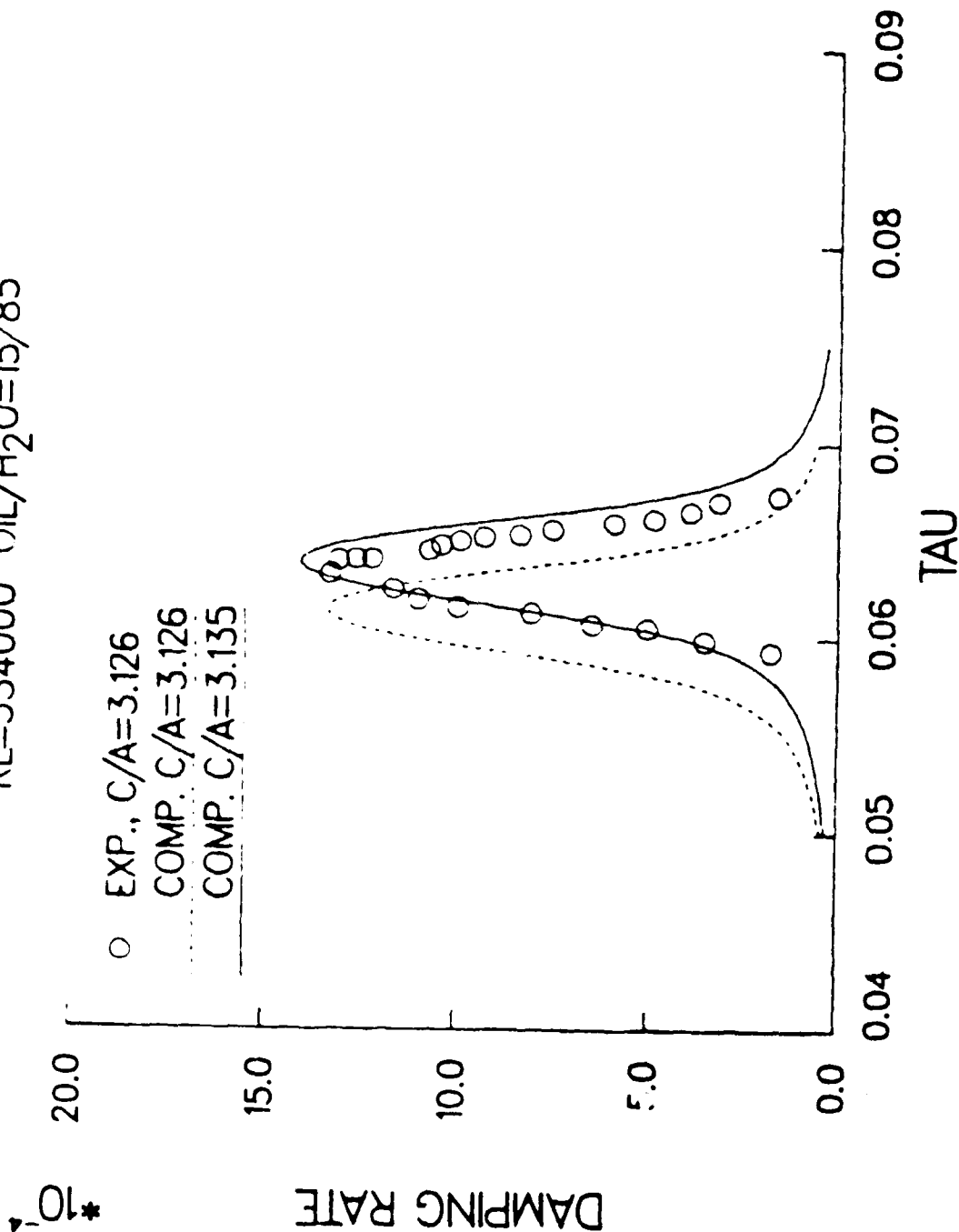


Figure 10. Damping Rate,  $-\epsilon\tau$ , versus  $\tau$  for  $Re_1 = 5.34 \times 10^5$ ,  $f = .89$ ,  $\nu_{21} = .812$ .

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APPENDIX A  
EFFECT OF CENTRAL ROD

# APPENDIX A. EFFECT OF CENTRAL ROD

The effect of a central rod on a single liquid payload has been discussed in detail by Fraser. <sup>A-1</sup> Conditions (2.19 - 2.21) at  $r = b_2$  are replaced by conditions similar to (2.22 - 2.24).

$$u_{2s}(b_2, x) = (s - i) (b_2/a) \hat{K}. \quad (A1)$$

$$v_{2s}(b_2, x) = -(s - i) (x/a) \hat{K}. \quad (A2)$$

$$w_{2s}(b_2, x) = i(s - i) (x/a) \hat{K}. \quad (A3)$$

Equation (A2), of course, replaces Eq. (5.3) as the boundary condition at  $r = b_2$ . Eqs. (4.16 - 4.17) are then replaced by

$$w_{2si}(b_2, x) + w_{21}\epsilon_2 + w_{22} = i(s - i) \hat{K}(x/a) \quad (A4)$$

$$u_{2si}(b_2, x) + u_{21}\epsilon_2 + u_{22} = (s - i) \hat{K}(b_2/a). \quad (A5)$$

A revised version of Table 2 can be computed for the viscous coefficient functions (see Table A1). For these viscous coefficient functions the only radial viscous velocity to be affected is that at  $r = b_2$  [Eq. (4.25)].

$$v_{2sv}(b_2, x) = (a/b_2) (v_{22} + \epsilon_2 v_{21}) \delta_{a2}. \quad (A6)$$

The inviscid boundary conditions now differ from Eqs. (5.1 - 5.4) by the condition at  $r = b_2$ . They are

at  $r = b_1$

$$p_{1si} + \frac{b_1 v_{1si}}{a(s - i)} = p_{21} \left[ p_{2si} + \frac{b_1 v_{2si}}{a(s - i)} \right] \quad (A7)$$

A1. J. L. Fraser and W. J. Scott, "Dynamics of a Liquid-Filled Shell: Unfilled Shell with a Central Rod," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Memorandum Report BRL-MR-1331, January 1959, 127 pages.

A2. J. L. Fraser, "Dynamics of a Liquid-Filled Shell: Viscous Effects in a Liquid-Filled Shell with a Central Rod," Ballistic Research Laboratory, Aberdeen Proving Ground, Maryland, BRL Memorandum Report BRL-MR-1959, January 1960, 127 pages.

TABLE A1. VISCOUS COEFFICIENT FUNCTIONS FOR CENTRAL ROD.

$$w_{10} = \{[1+N - (1-N) \epsilon_2^2] w_a + N \epsilon_1 \Delta w_{si}\} \hat{D}^{-1}$$

$$w_{11} = \{(1-N) \epsilon_1 w_a - N(1+\epsilon_2^2) \Delta w_{si} + 2 N \epsilon_2 w_b\} \hat{D}^{-1}$$

$$w_{21} = \{2 \epsilon_1 w_a + (1+\epsilon_1^2) \Delta w_{si} - \epsilon_2 (1-N) w_b\} \hat{D}^{-1}$$

$$w_{22} = \{-\epsilon_2 \Delta w_{si} + [1+N + (1-N) \epsilon_1^2] w_b\} \hat{D}^{-1}$$

$$u_{10} = \{[1+N - (1-N) \epsilon_2^2] u_a + N \epsilon_1 \Delta u_{si}\} \hat{D}^{-1}$$

$$u_{11} = \{(1-N) \epsilon_1 u_a - N(1+\epsilon_2^2) \Delta u_{si} + 2 N \epsilon_2 u_b\} \hat{D}^{-1}$$

$$u_{21} = \{2 \epsilon_1 u_a + (1+\epsilon_1^2) \Delta u_{si} - \epsilon_2 (1-N) u_b\} \hat{D}^{-1}$$

$$u_{22} = \{-\epsilon_2 \Delta u_{si} + [1+N + (1-N) \epsilon_1^2] u_b\} \hat{D}^{-1}$$

$$v_{10} = \{[1+N - (1-N) \epsilon_2^2] v_a + N \epsilon_1 \Delta^* \} \hat{D}^{-1}$$

$$v_{11} = \{-(1-N) \epsilon_1 v_a + N(1+\epsilon_2^2) \Delta^* - 2 N \epsilon_2 v_b\} \hat{D}^{-1}$$

$$v_{21} = \{2 \epsilon_1 v_a + (1+\epsilon_1^2) \Delta^* - \epsilon_2 (1-N) v_b\} \hat{D}^{-1}$$

$$v_{22} = \{\epsilon_2 \Delta^* - [1+N + (1-N) \epsilon_1^2] v_b\} \hat{D}^{-1}$$

where

$$\hat{D} = 1 + N + (1 - N) (\epsilon_1^2 - \epsilon_2^2)$$

$$w_b = i (s - i) (x/a) \hat{K} - w_{2si}(b_2, x)$$

$$u_b = (s - i) (b_2/a) \hat{K} - u_{2si}(b_2/x)$$

$$v_b = -(s - i) (x/a) \hat{K} - \left[ \frac{\partial (r v_{2si})}{\partial r} \right]_{r = b_2}$$

$$v_{1si} - v_{2si} + (1 - p_{21}) v_{2sv} \quad (A8)$$

at  $r = b_2$

$$v_{2si} + v_{2sv} = (i - s) (x/a) \hat{K} \quad (A9)$$

at  $r = a$

$$v_{1si} + v_{1sv} = (i - s) (x/a) \hat{K}, \quad (A10)$$

where the necessary viscous coefficient functions  $v_{jk}$  are given in Table A1.

It should be noted that in terms of  $\delta_{aj}$  the computational versions of Eqs. (A9-A10) which are used in this paper are slightly more accurate than those of Reference 3. For a single liquid they become

$$v_{si}(b_2, x) + \left[ \frac{b_2 a \delta_a}{b_2 + a \delta_a} \right] \frac{\partial v_{si}(b_2, x)}{\partial r} = (i - s) (x/a) \hat{K} \quad (A11)$$

$$v_{si}(a, x) - \left[ \frac{a \delta_a}{1 - \delta_a} \right] \frac{\partial v_{si}(a, x)}{\partial r} = (i - s) (x/a) \hat{K}. \quad (A12)$$

The corresponding equations of Reference 3 are:

$$v_{si}(b_2, x) + a \delta_a \frac{\partial v_{si}(b_2, x)}{\partial r} = (i - s) (x/a) \hat{K} \quad (A13)$$

$$v_{si}(a, x) - a \delta_a \frac{\partial v_{si}(a, x)}{\partial r} = (i - s) (x/a) \hat{K}. \quad (A14)$$

The difference between Eqs. (A11) and (A13) is only important when  $b_2$  is very small while the difference between Eqs. (A12) and (A14) is unimportant for Reynolds numbers appropriate to boundary layer theory.

After the usual substitutions of the Fourier series expansions, new forms of Eqs. (5.6 - 5.9) for the  $E_{jk}$ 's and  $F_{jk}$ 's can be obtained.

$$\begin{aligned}
R_{1k}(b_1) - \rho_{21} R_{2k}(b_1) - (b_1/a) (s - i)^{-1} [R_{v1k}(b_1) - \rho_{21} R_{v2k}(b_1)] \\
= \frac{(1 - \rho_{21}) s^2 (i - s)}{1 + s} (b_1/a) a_k
\end{aligned} \tag{A15}$$

$$R_{v1k}(b_1) - R_{v2k}(b_1) - (1 - \rho_{21}) \delta_{a2} \hat{R}_k^* = (1 - \rho_{21})(\epsilon_1 - \epsilon_2) \delta_{a2} \hat{A}_1 a_k \tag{A16}$$

$$\begin{aligned}
R_{v2k}(b_2) + a \delta_{a2} \hat{D} \hat{D}_2^{-1} R'_{v2k}(b_2) + (a/b_2) \epsilon_2 \delta_{a2} \hat{D}_2^{-1} R_k^{**} \\
= \frac{2s (i - s)}{1 + s} a_k
\end{aligned} \tag{A17}$$

$$R_{v1k}(a) - a \delta_{a1} \hat{A}_2 R'_{v1k}(a) + \epsilon_1 \delta_{a1} N \hat{D}_0^{-1} R_k^{**} = \frac{2s (i - s)}{1 + s} a_k, \tag{A18}$$

where

$$\begin{aligned}
\hat{R}_k^* &= \{a (1 + \epsilon_1^2 + \epsilon_2^2) [R'_{v1k}(b_1) - R'_{v2k}(b_1)] \\
&\quad - 2 (a/b_1) \epsilon_1 [R_{v1k}(a) + a R'_{v1k}(a)] \\
&\quad + 2 (a/b_1) \epsilon_2 [R_{v2k}(b_2) + b_2 R'_{v2k}(b_2)]\} \hat{D}_1^{-1} \\
\hat{A}_1 &= 4 (a/b_1) \left[ \frac{s (i - s)}{1 + s} \right] \hat{D}_1^{-1} \\
\hat{A}_2 &= [1 + N - (1 - N)(\epsilon_1^2 + \epsilon_2^2)] \hat{D}_0^{-1} \\
\hat{D}_0 &= \hat{D} - \delta_{a1} [1 + N - (1 - N)(\epsilon_1^2 + \epsilon_2^2)]
\end{aligned}$$

$$\hat{D}_1 = \hat{D} - \delta_{a2} (1 - \rho_{21})(1 + \epsilon_1^2 + \epsilon_2^2)(a/b_1)$$

$$\hat{D}_2 = \hat{D} + \delta_{a2} D (a/b_2).$$

The linear liquid moment coefficient for a cylinder with a central rod can be expressed as the sum of six terms--the four terms of Eq. (6.2) plus the pressure and viscous contributions from the central rod.

$$\tau (C_{LSM} + i C_{LIM}) = m_{p\ell} + m_{pe} + m_{pr} + m_{v\ell} + m_{ve} + m_{vr}. \quad (A19)$$

The two additional terms are quite similar to  $m_{p\ell}$  and  $m_{v\ell}$ , respectively.

$$m_{pr} = -i b_2 \rho_{21} (2a^2 c \hat{K})^{-1} \int_{-c}^c \tilde{x} [\tilde{p}_{2si}(b_2, \tilde{x}) + p_{2sv}(b_2, \tilde{x})] d\tilde{x}, \quad (A20)$$

$$\text{where } p_{2sv} = -2 \delta_{a2} (w_{22} - w_{21} \epsilon_2).$$

$$m_{vr} = N b_2 (2 a^2 c \hat{K} R_{e1} \delta_{a1})^{-1} \int_{-c}^c [i b_2 (u_{22} - \epsilon_2 u_{21}) + \tilde{x} (w_{22} - \epsilon_2 w_{21})] d\tilde{x}. \quad (A21)$$

In Figure A1 the maximum side moment coefficient associated with  $\tau_{31}$  is plotted versus  $b_1/a$  for the central rod of Figure 3. Note the sharp changes in side moment for the interface near the central rod and near the outer cylindrical wall. The two bumps in the  $\rho_{21} = .4$  curve are caused by the coalescence of the  $\tau_{31}$  and the  $\tau_{52}$  eigenfrequencies.

$Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = 0.98$   
Central Rod

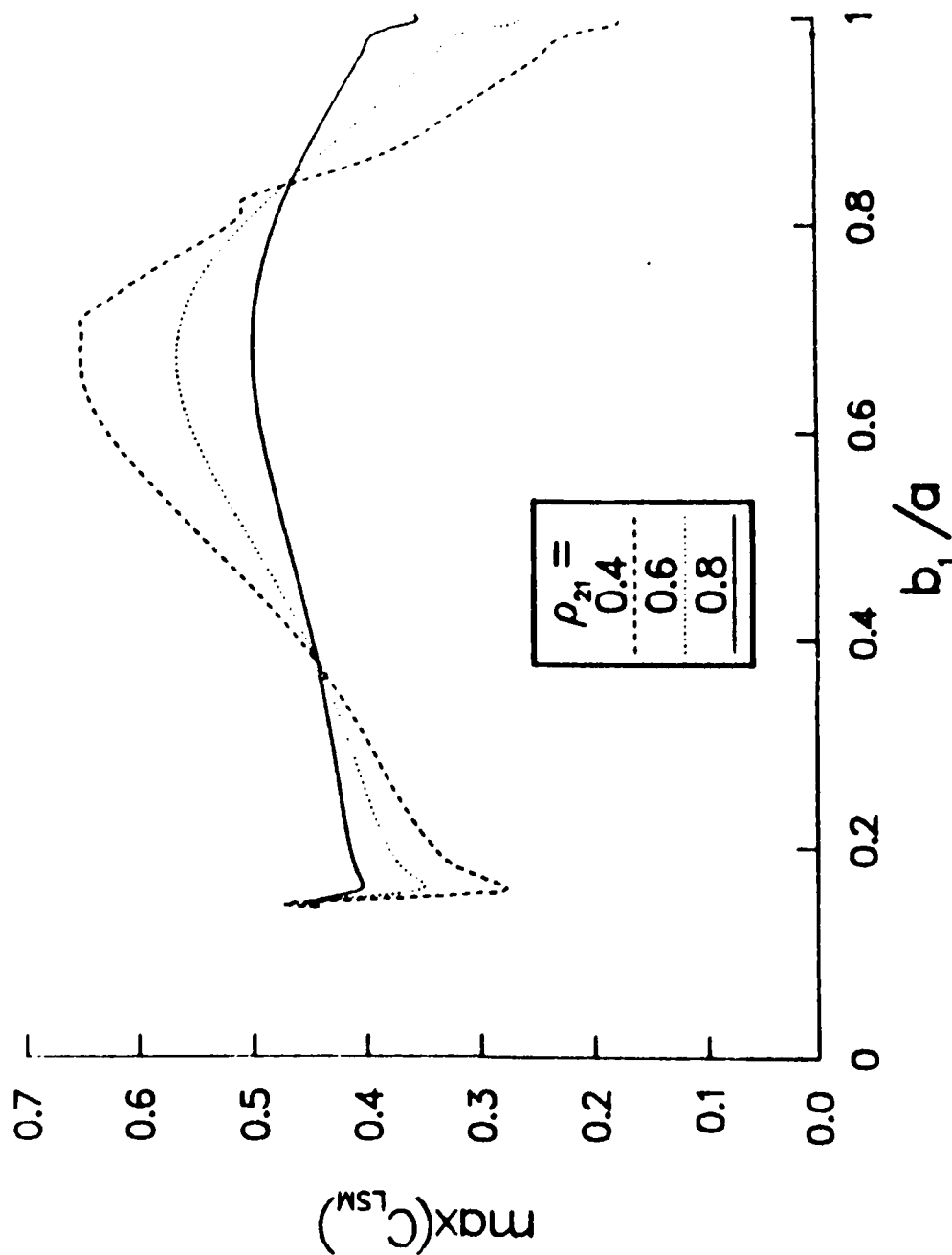


Figure A1.  $\tau_{31}$  Maximum Side Moment Coefficient versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = .98$  with a Central Rod and Various Density Ratios.



APPENDIX B  
EFFECT OF DIFFERENT KINEMATIC VISCOSITIES

## APPENDIX B. EFFECT OF DIFFERENT KINEMATIC VISCOSITIES

As was stated in the body of this report, the approximation given in Eq. (3.5) can be avoided by a much better least squares approximation. Exact expressions for  $p_{jsi}$ ,  $v_{jsi}$ , and  $v_{jsv}$  can be derived from the series of Table 1 and the other relations given in the main part of this report, and these are tabulated in Table B1. Next, these expressions for the pressure and radial velocity perturbation functions are substituted in Eqs. (5.1-5.4) to obtain four equations for the  $E_{kj}$ 's and  $F_{kj}$ 's:

$$\sum_k [E_{1k} A_{\ell k} + F_{1k} B_{\ell k}] \sin(\lambda_{1k} x/c) + \sum_k [E_{2k} C_{\ell k} + F_{2k} D_{\ell k}] \sin(\lambda_{2k} x/c) = d_{\ell} x/c \quad \ell = 1, 2, 3, 4 \quad (B1)$$

$$k = 1, 3, 5, 7, \dots, 2N_k - 1$$

where the coefficients  $A_{\ell k}$ ,  $B_{\ell k}$ ,  $C_{\ell k}$ ,  $D_{\ell k}$ ,  $d_{\ell}$  are given in Table B2.

For  $N_k$  sets of the parameters ( $E_{1k}$ ,  $E_{2k}$ ,  $F_{1k}$ ,  $F_{2k}$ ), these four equations can not be satisfied exactly. We can, however, consider the squared sum of the residuals for each equation produced by a particular selection:

$$R_{\ell}^2 = \int_{-c}^c \left| \sum_k [E_{1k} A_{\ell k} + F_{1k} B_{\ell k}] \sin(\lambda_{1k} x/c) + \sum_k [E_{2k} C_{\ell k} + F_{2k} D_{\ell k}] \sin(\lambda_{2k} x/c) - d_{\ell} x/c \right|^2 dx. \quad (B2)$$

We seek those values of the parameters  $E_{1k}$ ,  $E_{2k}$ ,  $F_{1k}$ ,  $F_{2k}$  that minimize (in a least squares sense) the  $R_{\ell}$ 's. For a single liquid and 100% fill ( $b_2 = 0$ ), the  $F_k$ 's satisfy the condition at  $r = b_2$  while the  $E_k$ 's satisfy the condition at  $r = a$ . For two liquids, the conditions at  $b_2$  and  $a$  are represented in Eqs. (B1-B2) by  $\ell = 3$  and  $4$ , respectively. Hence, in analogy with the simpler case, we select the  $F_{2k}$ 's to minimize  $R_3$  and the  $E_{1k}$ 's to minimize  $R_4$ . To satisfy the interface conditions ( $\ell = 1, 2$ ), we select the  $F_{1k}$ 's to minimize  $R_1$  and the  $E_{2k}$ 's to minimize  $R_2$ . The resulting  $4N_k$  equations are given in Table B3.

Tables B1 and B2 have to be modified for a fully-filled cylinder with a central rod of radius  $b_2$ . The pressure and inviscid radial velocity functions



in Table B1 are unchanged, but three viscous radial velocity functions have to be derived from Table A1 and are given in Table B4.

As was indicated in Appendix A, the boundary conditions at  $r = b_2$  for the free surface (Eq. (5.3)) is replaced by Eq. (A7). The corresponding Eq. (B1) is identified by  $\lambda = 3$ . The new coefficients are:

$$\begin{aligned} A_{3k} &= (a/b_2) \delta_{a2} h_{1k}^* \\ B_{3k} &= (a/b_2) \delta_{a2} h_{2k}^* \\ C_{3k} &= f_{2k}(b_2) + (a/b_2) \delta_{a2} h_{3k}^* \\ D_{3k} &= g_{2k}(b_2) + (a/b_2) \delta_{a2} h_{4k}^* \\ d_3 &= 2 s(i - s) (i + s)^{-1} - (a/b_2) \delta_{a2} h_1^*. \end{aligned} \tag{B4}$$

The remaining coefficients for  $\lambda = 1, 2, 4$  are given in Table B3 when the  $h_n$ ,  $h_{nk}$ 's of Table B4 are used.

As a comparison of approximation (Eq. 3.5) with the better approximation of this appendix, the maximum side moment coefficient for  $\tau_{31}$ ,  $Re = 40,000$ ,  $c/a = 3.1$ ,  $b_2 = 0$ ,  $\rho = 0.6$  is plotted versus  $b_1/a$  in Figure B1. Comparison of the two approximations are given for kinematic viscosity ratios ( $\nu_{21} = \nu_2/\nu_1$ ) of 0.1, 1, and 10. We see that approximation (Eq. 3.5) underestimates the effect of unequal kinematic viscosities.

$Re=40000, c/a=3.1, b_2=0, \rho_{21}=0.6$

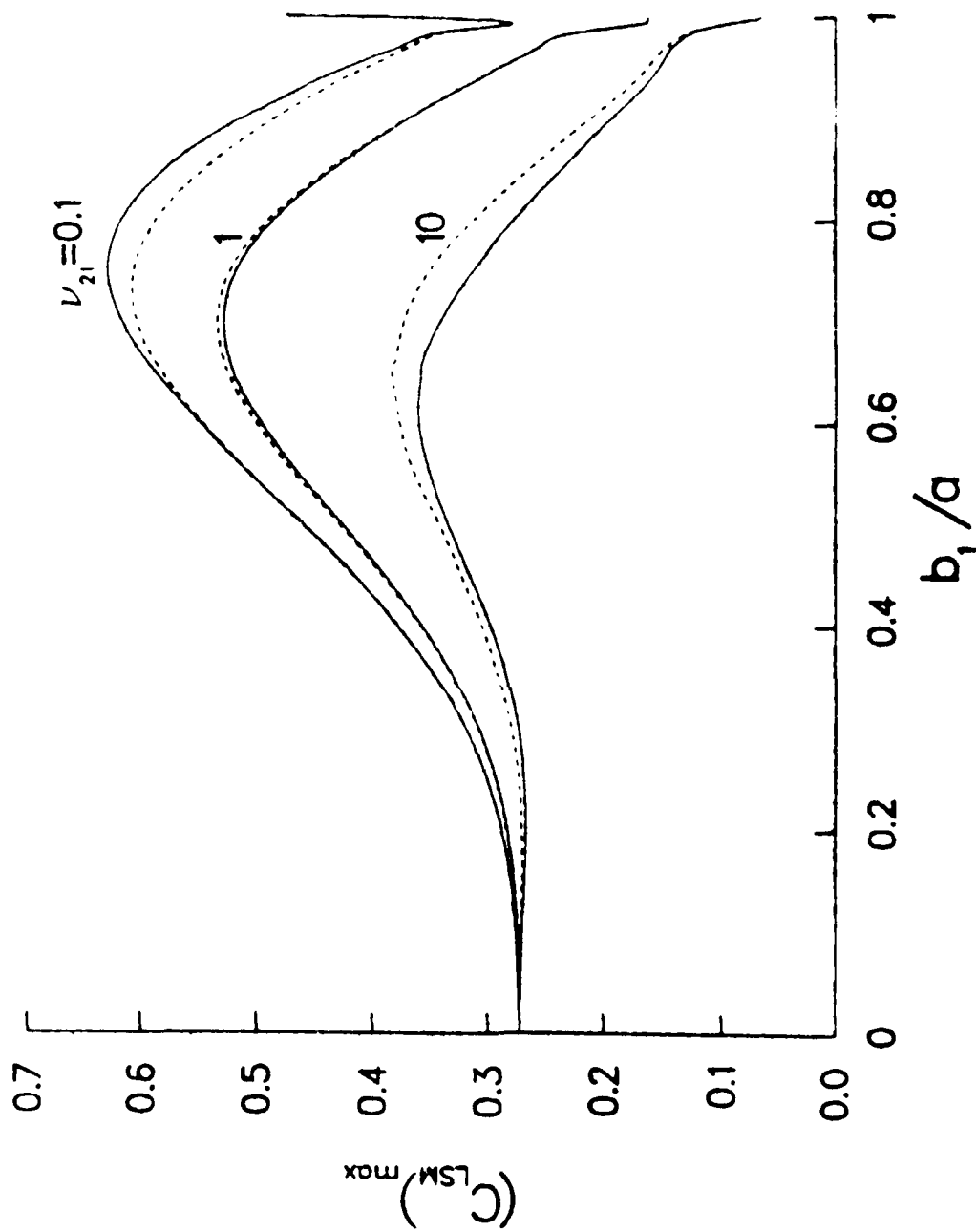


Figure B1.  $\tau_{31}$  Maximum Side Moment Coefficient versus  $b_1/a$  for  $Re_1 = 4 \times 10^4$ ,  $c/a = 3.1$ ,  $f = .98$ ,  $\rho_{21} = .6$  and Various Kinematic Viscosity Ratios. Using Average Viscosities Produces the Dashed Curves.

TABLE B1. PRESSURE AND RADIAL VELOCITY FUNCTIONS.

$$p_{jsi} = -(i-s)^2 (x/c)(r/a) + \sum [E_{jk} J_{1k}(\hat{r}) + F_{jk} Y_{1k}(\hat{r})] \sin(\lambda_{jk} x/c) \} (c/a) \hat{K}$$

$$v_{jsi} = \{ (i-s)^2 (i+s)^{-1} (x/c) + \sum [E_{jk} f_{jk}(r) + F_{jk} g_{jk}(r)] \sin(\lambda_{jk} x/c) \} (c/a) \hat{K}$$

$$v_{1sv}(a, x) = (h_1 x/c + \sum [E_{1k} h_{1k} + F_{1k} h_{2k}] \sin(\lambda_{1k} x/c) \\ + \sum [E_{2k} h_{3k} + F_{2k} h_{4k}] \sin(\lambda_{2k} x/c) \} (c/a) \delta_{a1} \hat{K}$$

$$v_{2sv}(b_1, x) = (h_2 x/c + \sum [E_{1k} h_{5k} + F_{1k} h_{6k}] \sin(\lambda_{1k} x/c) \\ + \sum [E_{2k} h_{7k} + F_{2k} h_{8k}] \sin(\lambda_{2k} x/c) \} (c/b_1) \delta_{a2} \hat{K}$$

where

$$\hat{r} = \lambda_{jk} r/c$$

$$f_{jk}(r) = -[(i-s) (a/c) \lambda_{jk} \frac{dJ_1(\hat{r})}{d\hat{r}} + 2i (a/r) J_1(\hat{r})] s^{-1}$$

$$g_{jk}(r) = -[(i-s) (a/c) \lambda_{jk} \frac{dY_1(\hat{r})}{d\hat{r}} + 2i (a/r) Y_1(\hat{r})] s^{-1}$$

$$h_1 = 2s [1 - 2\epsilon_1^2 (1 - N) D^{-1}] (i-s) (i+s)^{-1}$$

$$h_2 = 4\epsilon_1 s (i-s) (i+s)^{-1} D^{-1}$$

$$h_{1k} = -[1 - 2\epsilon_1^2 (1 - N) D^{-1}] \hat{f}_{1k}(a) + 2\epsilon_1 N D^{-1} \hat{f}_{1k}(b_1)$$

$$h_{2k} = -[1 - 2\epsilon_1^2 (1 - N) D^{-1}] \hat{g}_{1k}(a) + 2\epsilon_1 N D^{-1} \hat{g}_{1k}(b_1)$$

TABLE B1. PRESSURE AND RADIAL VELOCITY FUNCTIONS (Continued).

$$n_{3k} = -2 \epsilon_1 N D^{-1} \hat{f}_{2k}(b_1)$$

$$n_{4k} = -2 \epsilon_1 N D^{-1} \hat{g}_{2k}(b_1)$$

$$n_{5k} = -2 \epsilon_1 D^{-1} \hat{f}_{1k}(a) + (1 + \epsilon_1^2 - \epsilon_2^2) D^{-1} \hat{f}_{1k}(b_1)$$

$$n_{6k} = -2 \epsilon_1 D^{-1} \hat{g}_{1k}(a) + (1 + \epsilon_1^2 - \epsilon_2^2) D^{-1} \hat{g}_{1k}(b_1)$$

$$n_{7k} = -(1 + \epsilon_1^2 - \epsilon_2^2) D^{-1} \hat{f}_{2k}(b_1)$$

$$n_{8k} = -(1 + \epsilon_1^2 - \epsilon_2^2) D^{-1} \hat{g}_{2k}(b_1)$$

$$\hat{f}_{jk} = f_{jk} + r f'_{jk}$$

$$\hat{g}_{jk} = g_{jk} + r g'_{jk}$$

TABLE B2. COEFFICIENTS OF EQ. (B1).

$A_{1k} = J_1 (\hat{\lambda}_{1k} b_1/c) + (b_1/a) (i-s)^{-1} f_{1k} (b_1)$ $B_{1k} = Y_1 (\hat{\lambda}_{1k} b_1/c) + (b_1/a) (i-s)^{-1} g_{1k} (b_1)$ $C_{1k} = -\rho_{21} [J_1 (\hat{\lambda}_{2k} b_1/c) + (b_1/a) (i-s)^{-1} f_{2k} (b_1)]$ $D_{1k} = -\rho_{21} [Y_1 (\hat{\lambda}_{2k} b_1/c) + (b_1/a) (i-s)^{-1} g_{2k} (b_1)]$
$A_{2k} = (b_1/a) f_{1k} (b_1) - (1 - \rho_{21}) \delta_{a2} h_{5k}$ $B_{2k} = (b_1/a) g_{1k} (b_1) - (1 - \rho_{21}) \delta_{a2} h_{6k}$ $C_{2k} = -(b_1/a) f_{2k} (b_1) - (1 - \rho_{21}) \delta_{a2} h_{7k}$ $D_{2k} = -(b_1/a) g_{2k} (b_1) - (1 - \rho_{21}) \delta_{a2} h_{8k}$
$A_{3k} = B_{3k} = 0$ $C_{3k} = J_1 (\hat{\lambda}_{2k} b_2/c) + (b_2/a) (i-s)^{-1} f_{2k} (b_2)$ $D_{3k} = Y_1 (\hat{\lambda}_{2k} b_2/c) + (b_2/a) (i-s)^{-1} g_{2k} (b_2)$
$A_{4k} = f_{1k}(a) + \delta_{a1} h_{1k}$ $B_{4k} = g_{1k}(a) + \delta_{a1} h_{2k}$ $C_{4k} = \delta_{a1} h_{3k}; \quad D_{4k} = \delta_{a1} h_{4k}$
$d_1 = 0$ $d_2 = (1 - \rho_{21}) \delta_{a2} h_2$ $d_3 = s^2 (i - s) (i + s)^{-1} (b_2/a)$ $d_4 = 2s (i - s) (i + s)^{-1} - \delta_{a1} h_1$

$$r_{1k} = (-1)^k r_{1k}, \quad r_{2k} = (-1)^k r_{2k}, \quad r_{3k} = (-1)^k r_{3k}, \quad r_{4k} = (-1)^k r_{4k}.$$

$$[r_{1k} A_{1k} + r_{1k} B_{1k} + r_{2k} A_{2k} + r_{2k} B_{2k} + r_{3k} A_{3k} + r_{3k} B_{3k}] + d_1 b_m = 0$$

$$[r_{1k} A_{1k} + r_{1k} B_{1k} + r_{2k} A_{2k} + r_{2k} B_{2k} + r_{3k} A_{3k} + r_{3k} B_{3k}] + d_2 b_m = 0$$

$$[r_{1k} A_{1k} + r_{1k} B_{1k} + r_{2k} A_{2k} + r_{2k} B_{2k} + r_{3k} A_{3k} + r_{3k} B_{3k}] + d_3 b_m = 0$$

$$[r_{1k} A_{1k} + r_{1k} B_{1k} + r_{2k} A_{2k} + r_{2k} B_{2k} + r_{3k} A_{3k} + r_{3k} B_{3k}] + d_4 b_m = 0$$

$$m = 1, 3, 5, \dots, 2N_k - 1$$

where

$$b_{1k} = \frac{1}{C} \int_{-C}^C \sin(\bar{\lambda}_{1m} x/c) \sin(\lambda_{1k} x/c) dx$$

$$b_{2k} = \frac{1}{C} \int_{-C}^C \sin(\bar{\lambda}_{2m} x/c) \sin(\lambda_{2k} x/c) dx$$

$$b_{3k} = \frac{1}{C} \int_{-C}^C \sin(\bar{\lambda}_{1m} x/c) \sin(\lambda_{2k} x/c) dx$$

$$b_{4k} = \frac{1}{C} \int_{-C}^C \sin(\bar{\lambda}_{2m} x/c) \sin(\lambda_{1k} x/c) dx = \bar{b}_{km}$$

$$b_{1k} = \frac{1}{C} \int_{-C}^C x \sin(\bar{\lambda}_{1m} x/c) dx$$

$$b_{2k} = \frac{1}{C} \int_{-C}^C x \sin(\bar{\lambda}_{2m} x/c) dx$$



TABLE B4. VISCOUS RADIAL VELOCITY FUNCTIONS FOR CENTRAL ROD.

$$v_{1sv}(a,x) = \{h_1 x/c + \sum [E_{1k} h_{1k} + F_{1k} h_{2k}] \sin(\lambda_{1k} x/c) \\ + \sum [E_{2k} h_{3k} + F_{2k} h_{4k}] \sin(\lambda_{2k} x/c)\} (c/a) \delta_{a1} \hat{K}$$

$$v_{2sv}(b_1,x) = \{h_2 x/c + \sum [E_{1k} h_{5k} + F_{1k} h_{6k}] \sin(\lambda_{1k} x/c) \\ + \sum [E_{2k} h_{7k} + F_{2k} h_{8k}] \sin(\lambda_{2k} x/c)\} (c/b_1) \delta_{a2} \hat{K}$$

$$v_{2sv}(b_2,x) = \{h_1^* x/c + \sum [E_{1k} h_{1k}^* + F_{1k} h_{2k}^*] \sin(\lambda_{1k} x/c) \\ + \sum [E_{2k} h_{3k}^* + F_{2k} h_{4k}^*] \sin(\lambda_{2k} x/c)\} (c/b_2) \delta_{a2} \hat{K}$$

$$h_1 = 2s [1 - 2 \epsilon_1^2 (1 - N) \hat{D}^{-1}] (i - s) (i + s)^{-1}$$

$$h_2 = 4(\epsilon_1 - \epsilon_2) s (i - s) (i + s)^{-1} \hat{D}^{-1}$$

$$h_1^* = -2s [1 + 2 \epsilon_2^2 (1 - N) \hat{D}^{-1}] (i - s) (i + s)^{-1}$$

$$h_{1k} = -[1 - 2 \epsilon_1^2 (1 - N) \hat{D}^{-1}] \hat{f}_{1k}(a) + 2 \epsilon_1 N \hat{D}^{-1} \hat{f}_{1k}(b_1)$$

$$h_{2k} = -[1 - 2 \epsilon_1^2 (1 - N) \hat{D}^{-1}] \hat{g}_{1k}(a) + 2 \epsilon_1 N \hat{D}^{-1} \hat{g}_{1k}(b_1)$$

$$h_{3k} = -2 \epsilon_1 N \hat{D}^{-1} \hat{f}_{2k}(b_1)$$

$$h_{4k} = -2 \epsilon_1 N \hat{D}^{-1} \hat{g}_{2k}(b_1)$$

$$h_{5k} = -2 \epsilon_1 \hat{D}^{-1} \hat{f}_{1k}(a) + (1 + \epsilon_1^2 + \epsilon_2^2) \hat{D}^{-1} \hat{f}_{1k}(b_1)$$

TABLE B4. VISCOUS RADIAL VELOCITY FUNCTIONS FOR CENTRAL ROD (Continued).

$$u_{1k} = -2 \epsilon_1 \hat{D}^{-1} \hat{g}_{1k}(a) + (1 + \epsilon_1^2 + \epsilon_2^2) \hat{D}^{-1} \hat{g}_{1k}(b_1)$$

$$u_{2k} = -(1 + \epsilon_1^2 + \epsilon_2^2) \hat{D}^{-1} \hat{f}_{2k}(b_1) + 2 \epsilon_2 \hat{D}^{-1} \hat{f}_{2k}(b_2)$$

$$u_{3k} = -(1 + \epsilon_1^2 + \epsilon_2^2) \hat{D}^{-1} \hat{g}_{2k}(b_1) + 2 \epsilon_2 \hat{D}^{-1} \hat{g}_{2k}(b_2)$$

$$u_{1k}^* = 2 \epsilon_2 \hat{D}^{-1} \hat{f}_{1k}(b_1)$$

$$u_{2k}^* = 2 \epsilon_2 \hat{D}^{-1} \hat{g}_{1k}(b_1)$$

$$u_{3k}^* = [1 + 2 \epsilon_2^2 (1 - N) \hat{D}^{-1}] \hat{f}_{2k}(b_2) - 2 \epsilon_2 \hat{D}^{-1} \hat{f}_{2k}(b_1)$$

$$u_{4k}^* = [1 + 2 \epsilon_2^2 (1 - N) \hat{D}^{-1}] \hat{g}_{2k}(b_2) - 2 \epsilon_2 \hat{D}^{-1} \hat{g}_{2k}(b_1)$$

APPENDIX C  
AXISYMMETRIC EIGENVALUES



## APPENDIX C. AXISYMMETRIC EIGENVALUES

The eigenvalues of this report were determined by linear perturbation functions whose azimuthal variation was  $\exp(-i\theta)$ . A more general expression is  $\exp(-im\theta)$ . Since the boundary conditions have an azimuthal variation corresponding to  $m = 1$ , the steady-state response required a consideration of this value of  $m$  only. Experimental measurements of eigenfrequencies have been made for axisymmetric waves ( $m = 0$ ) in a single liquid.<sup>C1</sup> In this appendix we will derive the equations for axisymmetric waves in two liquids.

The inviscid perturbation functions for any  $m$  have been derived in Reference C2. In Table C1 the appropriate expressions are given for  $m \neq 1$ . The more general definitions for  $\alpha_{jm}$  and  $\beta_{jm}$ , also given in Reference C2, are

$$\alpha_{0m} = \frac{1 + i}{\sqrt{2(m+is)}} \text{Re}_j^{-1/2} \quad (C1)$$

$$\alpha_{jm} = -[2(m+is)]^{-1} [(2-m-is) \alpha_{jm}^{-1} - (2+m+is) \beta_{jm}^{-1}] \quad (C2)$$

$$\beta_{jm} = (c/a) [s - (2+m) i]^{1/2} \text{Re}_j^{1/2} \quad (C3)$$

$$\beta_{jm} = (c/a) [s + (2-m) i]^{1/2} \text{Re}_j^{1/2}, \quad (C4)$$

where the complex roots are selected to have positive real parts.

Since velocities at rigid boundaries are zero for  $m \neq 1$  perturbations, the corresponding viscous coefficient functions can be computed for an internal free surface from Table 2 when  $w_a$ ,  $u_a$ , and  $v_a$  are defined to be

$$w_a = -w_{1s}(\alpha, x). \quad (C5)$$

C1. J. J. Van der Linde, "Experimental Verification of the Inertia Oscillations of a Liquid in a Cylindrical Tank During Spin-up," HRL Contract Report 273, September 1964. Also in *Journal of Geophys. Astrophys. Fluid Dynamics*, Vol. 1, pp. 219-241.

C2. J. J. Van der Linde, "Steady Inertia of Liquid England During Spin-up Without a Free Surface," Aberdeen Research Laboratory, Aberdeen Proving Ground, Maryland, and Naval Research Office, AORL-TR-62541, August 1964. (All Rights Reserved)



TABLE C1. INVISCID PERTURBATION FUNCTIONS FOR  $m \neq 1$ .

$$p_{jsi} = - (c/a) \sum R_{jkm}(r) \sin (\lambda_{km} x/c) \hat{K}$$

$$u_{jsi} = (s - im)^{-1} \sum R_{jkm}(r) \lambda_{km} \cos (\lambda_{km} x/c) \hat{K}$$

$$v_{jsi} = (c/a) \sum R_{v jkm}(r) \sin (\lambda_{km} x/c) \hat{K}$$

$$w_{jsi} = (c/a) \sum R_{w jkm}(r) \sin (\lambda_{km} x/c) \hat{K}$$

$$R_{jkm} = E_{jkm} J_m (\hat{\lambda}_{km} r/c) + F_{jkm} Y_m (\hat{\lambda}_{km} r/c)$$

$$R_{v jkm} = [(s - im) a R'_{jkm} - 2 im (a/r) R_{jkm}] S_m^{-1}$$

$$R_{w jkm} = - [2 a R'_{jkm} + im (s - im) (a/r) R_{jkm}] S_m^{-1}$$

$$\hat{\lambda}_{km}^2 = S_m \lambda_{km}^2 (s - im)^{-2}$$

$$S_m = s^2 - 2 im s + 4 - m^2$$

$$u_a = - u_{1si} (a, x) \quad (C6)$$

$$v_a = - \left[ \frac{\partial (r v_{1si})}{\partial r} \right]_{r=a}. \quad (C7)$$

Table A1 can be used to compute viscous coefficient functions for a central rod and  $m \neq 1$  if, in addition to Eqs. (C5-C7), similar definitions are assigned to  $w_b$ ,  $u_b$  and  $v_b$ :

$$w_b = - w_{2si} (b_2, x) \quad (C8)$$

$$u_b = -u_{2s1}(b_2, x) \quad (C9)$$

$$v_b = - \left[ \frac{\partial (r v_{2s1})}{\partial r} \right]_{r=b_2} \quad (C10)$$

General versions of Eqs. (5.6-5.9) for  $m \neq 1$  can now be derived

$$R_{1km}(b_1) - \rho_{21} R_{2km}(b_1) - (b_1/a) [R_{v1km}(b_1) - \rho_{21} R_{v2km}(b_1)] (s - im)^{-1} = 0 \quad (C11)$$

$$R_{v1km}(b_1) - R_{v2km}(b_1) - (1 - \rho_{21}) \delta_{a2m} R_{km}^* = 0 \quad (C12)$$

$$R_{2km}(b_2) - (b_2/a) (s - im)^{-1} R_{v2km}(b_2) = 0 \quad (C13)$$

$$R_{v1km}(a) - A_1 \delta_{a1m} a R'_{v1km}(a) + \rho_{11} N \delta_{a1m} R_{km}^{**} D_0^{-1} = 0, \quad (C14)$$

where

$$R_{km}^* = [1 + \rho_1^2 + \rho_2^2] a [R'_{v1km}(b_1) - R'_{v2km}(b_1)] \\ + \rho_1 (a/b_1) [R_{v1km}(a) + a R'_{v1km}(a)] D_1^{-1}$$

$$R_{km}^{**} = [\delta_{a1m} D_1^{-1} + D_1 R'_{v1km}(b_1) - R_{v2km}(b_1) - b_1 R'_{v2km}(b_1)] .$$

Eqs. (C11-C14) have been coded for  $m = 0$  and eigenvalues can be computed. At least one nonsymmetric eigenfrequency measurement for  $Re = 43,000$  and  $Pr = 10$  is shown in Figure (1).  $\rho_{21}$  versus  $b_1/a$  is plotted for  $\rho_{21} = .4, .6$ , and the theoretical value for a single liquid is plotted for  $b_1/a = 0, 1$ .

$Re = 43000, c/a = 0.995, m = 0, k = 2, b_2 = 0$

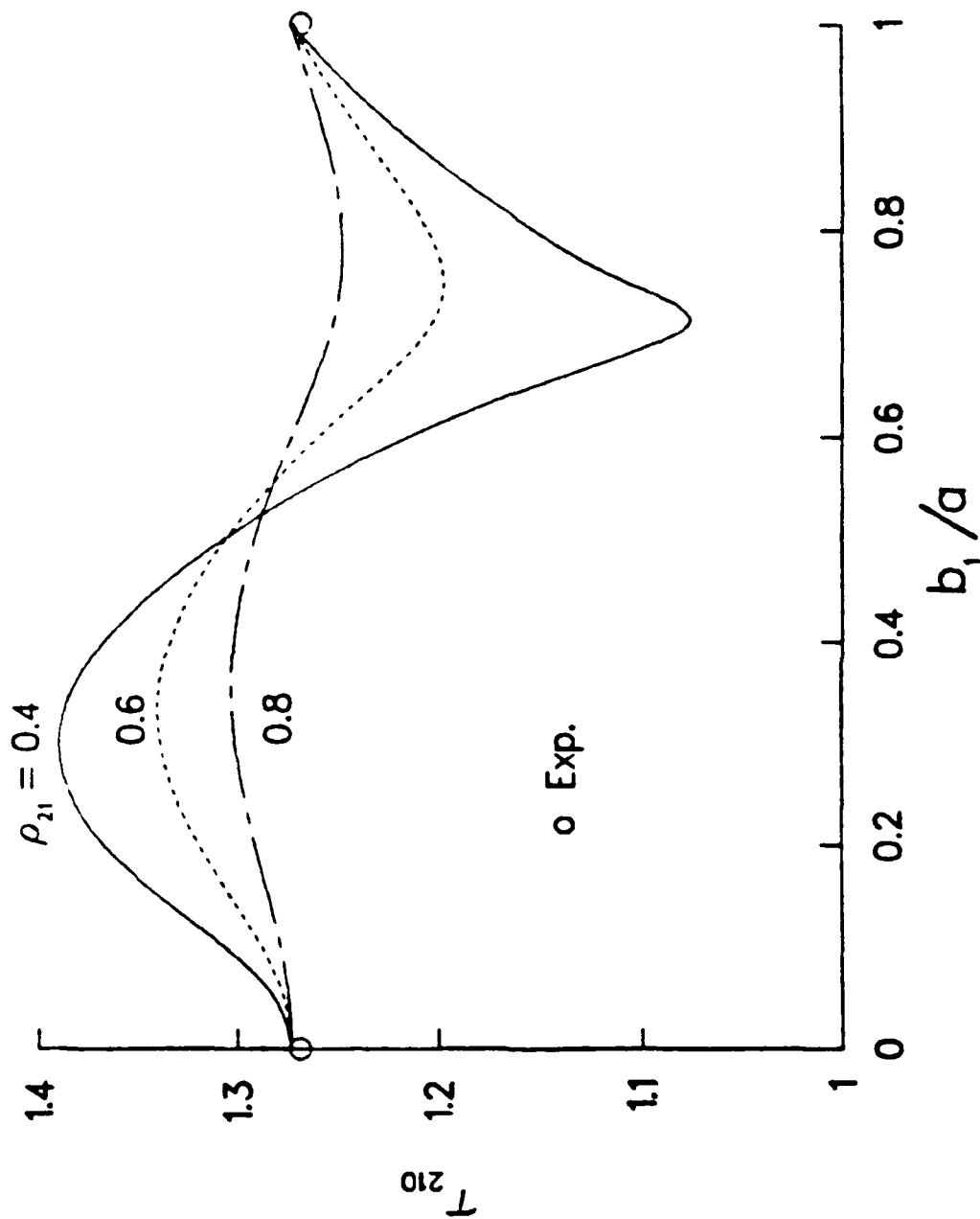


Figure C1.  $\tau_{210}$  versus  $b_1/a$  for  $Re_1 = 4.3 \times 10^4, c/a = 0.995, f = 1, m = 0$  and Various Density Ratios.

# LIST OF SYMBOLS

$a$	radius of the cylindrical cavity containing the liquids
$a_k$	coefficients in a least squares fit of $x/c$ to a series in $\sin(\lambda_k x/c)$ , Eq. (5.5)
$b_1$	radius of the interface of the two liquids for $K_1 = 0$
$b_2$	radius of an air core (or central rod) for $K_1 = 0$
$c$	half-height of the cylindrical cavity containing the liquids
$f$	$1 - (b_2/a)^2$ , the fill ratio
$m_L$	$2\pi\rho_1 a^2 c$ , the liquid mass in the cavity fully filled with liquid 1
$m_{pe}$	pressure moment coefficient on the end walls, Eq. (6.5)
$m_{pe}$	pressure moment coefficient on the lateral wall, Eq. (6.4)
$m_{pr}$	pressure moment coefficient on the lateral wall, Eq. (A20)
$m_{ve}$	viscous moment coefficient on the end walls, Eq. (6.7)
$m_{ve}$	viscous moment coefficient on the lateral wall, Eq. (6.6)
$m_{vr}$	viscous moment coefficient on the lateral wall due to a rod, Eq. (A21)
$p$	liquid pressure
$p_{js}$	pressure perturbation in liquid $j$
$p_{js}^i$	inviscid part of $p_{js}$



# LIST OF SYMBOLS (Continued)

$\tilde{p}_{jsi}$	$p_{jsi} - (\tilde{r} \tilde{x}/a^2) \hat{k}$
$p_{jsv}$	viscous part of $p_{js}$
$r$	radial coordinate in the inertial system
$\tilde{r}$	radial coordinate in the aeroballistic system
$s$	$(\epsilon + i)\tau$
$s_{kn}$	eigenvalues of $s$ : the values of $s$ that make the determinant of the system (5.6-5.9) zero
$t$	time
$u_{jin}$	coefficients in the expansion of $u_{jsv}$ , Eqs. (4.6-4.7)
$u_{js}, v_{js}, w_{js}$	$x, r, \theta$ components of the liquid $j$ velocity perturbation
$u_{jsi}, v_{jsi}, w_{jsi}$	inviscid part of $u_{js}, v_{js}, w_{js}$
$u_{jsv}, v_{jsv}, w_{jsv}$	viscous part of $u_{js}, v_{js}, w_{js}$
$w_{jk}$	coefficients in the expansion of $w_{jsv}$ , Eqs. (4.4-4.5)
$x$	axial coordinate in the inertial system
$\tilde{x}$	axial coordinate in the aeroballistic system
$C_{LIM}$	liquid in-plane moment coefficient, defined by Eq. (6.1)
$C_{LSM}$	liquid side moment coefficient, defined by Eq. (6.1)
$E_{jk}, F_{jk}$	coefficients in the expression for $R_{jk}$ computed by solving the system (5.6-5.9)

# LIST OF SYMBOLS (Continued)

$J_1$	Bessel function of the first kind of order 1
$\hat{K}$	$K_1(0) e^{i\theta_1(0)}$
$K_1(t)$	amplitude of the coning motion
$N$	$\rho_{21} (\nu_2/\nu_1)^{1/2}$
$N_k$	number of terms considered in summing for $k = 1, 3, 5 \dots (2 N_k - 1)$
$M_{L\tilde{Y}}, M_{L\tilde{Z}}$	$\tilde{Y}, \tilde{Z}$ components of the liquid moment, Eq. (6.1)
$Re_j$	$a^2 \phi^2 \nu_j^{-1}$ , Reynolds number for liquid j
$R_{jk}$	$E_{jk} J_1(\hat{\lambda}_k r/c) + F_{jk} Y_1(\hat{\lambda}_k r/c)$
$R_{vjk}$	$[(s - i) a R'_{jk} - 2 i (a/r) R_{jk}] S^{-1}$
$R_{wjk}$	$-[2 a R'_{jk} + i (s - i) (a/r) R_{jk}] S^{-1}$
$S$	$s^2 - 2is + 3$
$V_{x,j}, V_{r,j}, V_{\theta,j}$	$x, r, \theta$ components of the liquid j velocity, Eqs. (2.7-2.9)
$x, y$	inertial system Cartesian axes, the X-axis tangent to the trajectory at time zero
$\tilde{x}, \tilde{y}$	aeroballistic system Cartesian axes, the $\tilde{X}$ -axis along the missile's axis of symmetry
$Y_1$	Bessel function of the second kind of order 1

# LIST OF SYMBOLS (Continued)

$\tilde{\alpha}$	angle of attack: the projection in the $\tilde{X}\tilde{Z}$ plane of the angle between the $X$ and $\tilde{X}$ axes
$\tilde{\beta}$	angle of sideslip: the projection in the $\tilde{X}\tilde{Y}$ plane of the angle between the $X$ and $\tilde{X}$ axes
$\delta_{aj}$	$\left[ \frac{1+i}{\sqrt{2}(1+is)} \right] \text{Re}_j^{-1/2}$
$\delta_{cj}$	$-\frac{(a/c)(1+i)}{2\sqrt{2}(1+is)} \left[ \frac{1-is}{\sqrt{3+is}} + \frac{i(3+is)}{\sqrt{1-is}} \right] \text{Re}_j^{-1/2}$
$\Delta p_j$	fluctuating part of the inviscid pressure, Eq. (6.3)
$\dot{\epsilon}$	$(K_1/K_1) \dot{\phi}_1^{-1}$ , non-dimensionalized damping
$\epsilon_1$	$\exp [(b_1-a)/a \delta_{a1}]$
$\epsilon_2$	$\exp [(b_2-b_1)/a \delta_{a2}]$
$\eta_j$	dimensionless perturbation of liquid interfaces due to coning motion, Eqs. (2.5-2.6)
$\theta$	azimuthal coordinate in the inertial system
$\tilde{\theta}$	azimuthal coordinate in the aeroballistic system
$\lambda_k$	"average" value of $\lambda_{jk}$ , Eq. (3.5)
$\lambda_{jk}$	$(\pi k/2) (1 + \delta_{cj})$
$\hat{\lambda}_{jk}$	$[S^{1/2}/(1+is)] \lambda_{jk}$

# LIST OF SYMBOLS (Continued)

$\nu_j$	$\rho_j$ , dynamic viscosity of liquid j
$\nu_a$	average kinematic viscosity, Eq. (3.5)
$\nu_j$	kinematic viscosity of liquid j
$\rho_j$	density of liquid j
$\rho_2/\rho_1 \leq 1$	
$\dot{\phi}_1/\dot{\phi}$	nondimensionalized frequency
$s_{kn}$	eigenfrequency for modes k and n; the imaginary part of $s_{kn}$
$\dot{\phi}t$	
$\dot{\phi}$	inertia spin rate
$\phi_1(t)$	phase angle of the coning motion

## Derivatives:

$(\dot{\phantom{x}})$	$d(\phantom{x})/dt$
$(\phantom{x})'$	$d(\phantom{x})/dr$

## Indices:

e	endwall
i	liquid no. (1 heavier, 2 lighter)
k	axial mode number: 1,3,5,...(2 $N_k$ - 1)
l	lateral wall
n	radial mode number: 1,2,3,....
p	pressure component
v	viscous (wall shear) component

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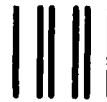
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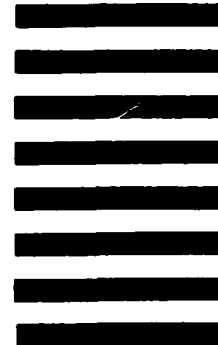


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